

## Supporting Information

# Selection of Ionic Liquids to be used as Separation Agents for Terpenes and Terpenoids

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## Experimental Section

**Chemicals.** The individual samples of the ILs used were purified under vacuum (0.1 Pa and 353 K) and constant stirring, for at least 48 h. The purity was then analysed using  $^1\text{H}$ ,  $^{13}\text{C}$ , and  $^{19}\text{F}$  NMR spectra. In order to further reduce the water traces and the volatile impurities, ILs individual samples were additionally dried during 72 hours at 300 K under reduced pressure. Karl-Fischer titration was used to determine the water content of the dry ILs. For that, samples were dissolved in dry methanol and titrated with a step of 2.5  $\mu\text{L}$ . The water content was found to be below 300 ppm for all IL samples. Terpenes and terpenoids were used without any further purification since the GLC technique operates at elevated temperatures ( $> 398.15\text{ K}$ ) and thus, impurities can be removed from the column.

**Apparatus and Experimental Procedure.** The infinite dilution activity coefficients were estimated from retention times measurements performed using a PerkinElmer Clarus 500 gas chromatograph through the GLC method. Experimental data were collected and treated using the TotalChrom Workstation software. The chromatograph injector and detector were kept at 473.15 K during the experiments. The carrier gas chosen was helium since it gives greater sensitivity to the TCD detector. The exit gas flow rate and the outlet pressure,  $P_0$ , were both measured with one Agilent Precision Gas Flow Meter placed after the detector, with uncertainties of  $\pm 0.1\text{ cm}^3\cdot\text{min}^{-1}$  and  $\pm 0.07\text{ kPa}$ , respectively. The inlet pressure,  $P_i$ , was measured by the gas chromatograph, through a pressure gauge, with an uncertainty of  $\pm 0.1\text{ kPa}$ . The settled inlet pressure was 80 kPa while the outlet pressure ranged between [97.84 – 100.18] kPa. The columns were prepared using the rotary evaporation technique, described before.<sup>1,2</sup> For the packing, between 45w% to 55w% of the IL stationary phase was used, along with a 100–120 mesh Chromosorb W/AW – DMCS solid support material (supplied by Sigma-Aldrich). The stationary phase and the solid support were weighed with a precision of  $\pm 1 \times 10^{-4}\text{ g}$ . High amounts of ILs were utilized in order to prevent the residual adsorption effects of the solutes on the solid support. Methanol was used as solvent in order to promote the ionic liquid coating onto Chromosorb. After that the methanol was evaporated using a vacuum-assisted rotary evaporator and the dry packing was used to fill glass columns of 1 m length and 4 mm internal diameter. The final columns were subsequently placed in the chromatograph and a stream of helium gas

was passed through the stationary phase during 6 h (388 K and 60 kPa) for the final drying. Large amounts of column packing are used to avoid the residual adsorption of solute onto the column packing. At least two columns with different packing percentage were prepared for each IL, the repeatability of  $\gamma_{13}^{\infty}$  values from two columns were within  $\pm 1.5\%$  for the vast majority of the solutes. Retention times were measured injecting in the column volumes of (0.01 to 0.3)  $\mu\text{L}$  of the different solutes together with air, a completely non-retained component. Small volumes of solutes were injected to be at infinite dilution conditions. The retention time of air corresponds to the dead time value,  $t_G$ , that was also measured. Each experiment was repeated at least two times in order to check the repeatability that was found to be within 0.01 – 0.03 min depending upon the temperature and the solute. The minimum and maximum absolute values of retention times were found to be 0.04 and 249.72 min corresponding to  $\alpha$ -pinene and carvacrol, respectively. During the measurements the column temperature was controlled by the gas chromatograph ( $\pm 0.02$  K). Considering the solute retention times accuracy ( $\pm 0.01$  min), and the standard deviations (in parentheses) related with: solute vapor pressures ( $< 5\%$ ), mass of the stationary phase ( $< 1 \times 10^{-4}$  g), flow rate of helium ( $0.1 \text{ cm}^3 \cdot \text{min}^{-1}$ ), inlet (0.1 kPa) and outlet (0.07 kPa) pressures, and oven temperature (0.02 K); the uncertainties in  $\gamma_{13}^{\infty}$  were estimated by error propagation to be less than 3%.

**COSMO-RS.** COSMO-RS is a well-established *a priori* method to predict thermophysical properties of fluids and liquid mixtures based on unimolecular quantum calculations. Theoretical details about this method can be found elsewhere.<sup>3-5</sup> To predict the  $\gamma_{13}^{\infty}$  with COSMO-RS first it is necessary to generate distinct input files, for terpenes and terpenoids and IL cations and anions, using BP functional B88-p86 with a triple- $\xi$  valence polarized basis set (TZVP) and the resolution of identity standard (RI) approximation using TURBOMOLE 6.1 program package.<sup>6</sup> The following calculation consist mainly of statistical thermodynamics and were performed using COSMOtherm, which provides an efficient and flexible implementation of the COSMO-RS method. The parameterization adopted was BP\_TZVP\_C30\_1401 (COSMOconfX v3.0, COSMOlogic GmbH & Co KG, Leverkusen, Germany). It contains intrinsic parameters of COSMOtherm and element specific parameters, required for the calculation of physiochemical data. In all calculation, ILs have been described by an equimolar mixture of the cation and the anion, that contribute  $\sigma$ -profile as two different compounds, allowing the study of specific

contribution of each counter ion. As consequence, it is necessary to scale the calculated values with the factor 0.5.<sup>5</sup> Moreover, the lowest energy conformations of all the species involved were used in the COSMO-RS calculations.

### Theoretical Basis

In 1960s, Everett<sup>7</sup> and Cruickshank et al.<sup>8</sup> developed a relation to calculate the activity coefficient at infinite dilution for a solute (1) partitioning between a carrier gas (2) and a non-volatile liquid solvent (3) through the solute retention,

$$\ln \gamma_{13}^{\infty} = \ln \left( \frac{n_3 RT}{V_N P_1^*} \right) - \frac{P_1^* (B_{11} - V_1^*)}{RT} + \frac{P_0 J_2^3 (2B_{12} - V_1^{\infty})}{RT} \quad (\text{S1})$$

where  $n_3$  refers to the number of moles of solvent (IL) on the column packing,  $T$  is the column/oven temperature,  $V_N$  is the net retention volume of the solute,  $P_1^*$  is the saturated vapour pressure of the solute,  $B_{11}$  is the second virial coefficient of the pure solute,  $V_1^*$  is the molar volume of the solute,  $P_0$  is the outlet pressure,  $J_2^3$  is a pressure correction term,  $B_{12}$  is the mixed second virial coefficient of the solute and the carrier gas (helium), and  $V_1^{\infty}$  is the partial molar volume of the solute at infinite dilution in the solvent. The temperature dependent properties are calculated at  $T$ . The standard state for the solute is pure liquid at system temperature and zero pressure.

The pressure correction term,  $J_2^3$ ,<sup>9</sup> and the net retention volume of the solute,  $V_N$ , are given by:

$$J_2^3 = \frac{2 (P_i / P_0)^3 - 1}{3 (P_i / P_0)^2 - 1} \quad (\text{S2})$$

$$V_N = (J_2^3)^{-1} U_0 (t_R - t_G) \quad (\text{S3})$$

where  $t_R$  and  $t_G$  are the retention times for the solute and the unreturned gas (air), respectively.  $U_0$  is the column outlet volumetric flow rate, corrected for the vapour pressure of water by,

$$U_0 = U \left( 1 - \frac{P_w}{P_0} \right) \frac{T}{T_f} \quad (\text{S4})$$

where  $T_f$  and  $U$  are, respectively, the temperature and the volumetric flow rate, both measured outside the column, and  $P_w$  is the vapour pressure of water at  $T_f$ .

The properties required for the  $\gamma_{13}^\infty$  calculations are presented in Table S1, as well as literature sources and methods applied in their estimation. The virial coefficients were calculated using the correlation proposed by Tsonopolous,<sup>10</sup> available in Poling and Prausnitz.<sup>11</sup>

In order to interpret the interactions and the measured  $\gamma_{13}^\infty$  data, partial molar excess thermodynamic functions at infinite dilution, namely the Gibbs free energy ( $\overline{G}_m^{E,\infty}$ ), enthalpy ( $\overline{H}_m^{E,\infty}$ ) and entropy ( $\overline{S}_m^{E,\infty}$ ), were calculated through the following equations:

$$\overline{G}_m^{E,\infty} = RT \ln(\gamma_{13}^\infty) \quad (\text{S5})$$

$$\overline{H}_m^{E,\infty} = R \left( \frac{\partial \ln \gamma_{13}^\infty}{\partial (1/T)} \right)_{p,x} \quad (\text{S6})$$

$$\overline{S}_m^{E,\infty} = \frac{\overline{H}_m^{E,\infty} - \overline{G}_m^{E,\infty}}{T} \quad (\text{S7})$$

where subscripts  $p$  and  $x$  indicate isobaric condition and constant composition, respectively.

Aiming at obtaining information about the recovery of terpenes and terpenoids from ionic liquid mixtures, the gas–liquid partition coefficients  $K_L = (c_1^L / c_1^G)$  for a solute partitioning between the carrier gas (helium) and the stationary phase (IL), were calculated according to,<sup>12</sup>

$$\ln(K_L) = \ln \left( \frac{V_N \rho_3}{m_3} \right) - \frac{P_0 J_2^3 (2B_{12} - V_1^\infty)}{RT} \quad (\text{S8})$$

being  $\rho_3$  the density and  $m_3$  the mass of the IL.

Lastly, to evaluate the performance of ILs as solvents for several practical chemical separation problems, the selectivity between the solutes  $i$  and  $j$ ,  $S_{ij}^\infty$ , and the separation process capacity,  $k_j^\infty$ , are determined as follow:<sup>13</sup>

$$S_{ij}^\infty = \gamma_i^\infty / \gamma_j^\infty \quad (\text{S9})$$

$$k_j^\infty = 1 / \gamma_j^\infty \quad (\text{S10})$$

where  $j$  is the solute that presents the smaller  $\gamma_{i3}^\infty$  in the solvent (ILs).

**Table S1.** Vapor pressures coefficients<sup>a</sup>, densities coefficients<sup>b</sup>, critical properties<sup>c</sup>, acentric factors<sup>c</sup> and dipole moments<sup>d</sup> of the terpenes and terpenoids studied.

Solutes	Vapor Pressure					Density					Critical Properties			Acentric Factor $\omega$	Dipole Moment $\mu / \text{C m}$
	$p = 10^{(A-B/(T+C))}$ , p/Pa, T/K					$\rho = A \cdot T^2 + B \cdot T + C$ , $\rho/\text{kmol} \cdot \text{m}^{-3}$ , T/K					$T_c$ , K	$V_c$ , $\text{cm}^3/\text{mol}$	$P_c$ , Pa		
	A	B	C	$T_{\min}$	$T_{\max}$	A	B	C	$T_{\min}$	$T_{\max}$					
$\alpha$ -pinene	9.325	1636.919	-48.140	238.19	308.15	-2.001E-06	-4.866E-03	7.905	278.16	368.14	630.78	484.50	2.891E+06	0.326	1.163E-30
$\beta$ -pinene	9.344	1687.684	-47.835	248.13	308.15	-1.446E-06	-5.050E-03	7.996	278.16	368.14	646.03	482.50	2.884E+06	0.320	4.022E-30
(-)-borneol	14.261	4288.902	13.509	273.65	308.15	6.425E-07	-7.641E-04	6.455	473.15	523.15	670.24	514.50	3.167E+06	0.698	7.215E-30
(-)-isopulegol	9.876	1981.013	-65.493	260.00	340.00	-9.100E-07	-4.831E-03	7.393	278.16	368.14	656.76	527.50	2.770E+06	0.698	9.703E-30
(-)-menthone	8.846	1499.364	-93.462	372.00	397.00	-4.033E-07	-4.810E-03	7.240	278.16	368.14	689.70	528.50	2.595E+06	0.412	1.450E-29
(1R)-(-)-fenchone	9.684	1936.425	-46.047	243.15	308.15	-5.096E-07	-5.228E-03	7.784	283.16	368.14	679.18	503.50	3.083E+06	0.388	1.466E-29
(R)-(+)-camphor	9.082	1650.630	-75.596	257.35	709.00	0.000E+00	-1.793E-02	13.894	477.15	480.57	700.16	503.50	3.083E+06	0.388	1.533E-29
(S)-(+)-carvone	10.048	2364.370	-31.980	320.00	511.00	-4.877E-07	-5.046E-03	7.922	278.16	368.14	724.81	503.50	2.860E+06	0.419	1.779E-29
Carvacrol	10.342	2549.857	-32.705	343.00	510.00	-2.735E-06	-3.413E-03	7.733	279.51	368.14	722.20	447.50	3.440E+06	0.581	6.273E-30
DL-citronellol	9.909	2045.850	-79.149	341.98	554.17	-3.210E-06	-2.545E-03	6.512	279.85	368.14	657.87	589.50	2.448E+06	0.848	7.863E-30
Eucalyptol	9.382	1725.544	-52.393	253.15	308.15	-9.128E-07	-5.033E-03	7.550	278.16	368.14	661.05	509.50	3.019E+06	0.339	8.034E-30
Eugenol	10.081	2457.820	-42.580	351.00	530.00	-5.632E-07	-5.039E-03	8.022	278.16	368.14	735.58	444.50	3.581E+06	0.676	1.181E-29
Geraniol	10.730	2773.110	-18.707	277.15	503.15	-3.161E-06	-2.790E-03	6.796	288.16	368.14	671.67	576.50	2.571E+06	0.820	1.185E-29
L(-)-menthol	10.383	2405.948	-37.850	329.15	485.15	-5.486E-06	-1.239E-03	6.578	318.16	358.14	661.63	539.50	2.660E+06	0.716	7.842E-30
Linalool	4.556	341.017	-183.210	368.00	428.00	-3.680E-06	-3.230E-03	6.852	280.01	368.14	633.30	565.50	2.582E+06	0.755	9.673E-30
Thymol	10.294	2522.332	-28.575	337.40	504.90	-2.607E-06	-3.614E-03	7.766	328.16	368.14	715.83	447.50	3.440E+06	0.581	6.291E-30
$\alpha$ -pinene oxide	7.758	975.321	-127.664	298.15	482.00	-9.571E-07	-4.906E-03	7.861	278.16	368.14	716.40	489.50	3.093E+06	0.369	9.757E-30

<sup>a</sup>References:  $\alpha$ -pinene,<sup>14</sup>  $\beta$ -pinene,<sup>14</sup> (-)-borneol,<sup>15</sup> (-)-isopulegol: not publish yet, (-)-menthone,<sup>16</sup> (1R)-(-)-fenchone,<sup>15</sup> (R)-(+)-camphor,<sup>17</sup> (S)-(+)-carvone,<sup>18</sup> Carvacrol,<sup>19</sup> DL-citronellol,<sup>17</sup> Eucalyptol,<sup>20</sup> Eugenol,<sup>18</sup> Geraniol,<sup>17</sup> L(-)-menthol,<sup>21</sup> Linalool,<sup>22</sup> Thymol,<sup>19</sup>  $\alpha$ -pinene oxide;<sup>23-25</sup> <sup>b</sup>Reference;<sup>26</sup> <sup>c</sup>Estimated using

the Joback group-contribution method;<sup>27,28</sup> <sup>d</sup>Estimated using TURBOMOLE 6.1 programme package on the density functional theory level, utilizing the BP functional B88-P86 with a triple- $\zeta$  valence polarized basis set (TZVP) and the resolution of identity standard (RI) approximation.<sup>6</sup>



**Table S2.** Experimental activity coefficients at infinite dilution of terpenes and terpenoids in ILs, at different temperatures.<sup>a</sup>

Solutes	T/K	[C <sub>4</sub> mim]Cl <sup>b</sup>						[C <sub>4</sub> mim][CH <sub>3</sub> SO <sub>3</sub> ] <sup>c</sup>					
		398.15	408.15	418.15	428.15	438.15	448.15	398.15	408.15	418.15	428.15	438.15	448.15
$\alpha$ -pinene	301.13	279.40	266.50	252.23	237.17	225.94	59.41	57.88	56.08	54.21	52.58	51.15	
$\beta$ -pinene	210.73	201.65	195.20	188.20	182.73	176.27	43.19	42.43	41.67	40.97	40.23	39.53	
(-)-borneol	3.60	3.32	3.06	2.84	2.54	2.30							
(-)-Isopulegol	7.87	8.42	8.97	9.34	9.88	10.22	3.78	3.98	4.13	4.29	4.40	4.52	
(-)-menthone	90.84	91.53	91.08	90.86	90.42	88.74	17.33	17.46	17.44	17.39	17.37	17.40	
(1R)-(-)-fenchone	63.56	62.09	61.24	59.35	57.54	57.58	12.58	12.55	12.36	12.27	12.16	12.05	
(1R)-(+)-camphor	50.74	51.46	51.49	51.58	51.61	51.12	10.71	10.78	10.81	10.85	10.87	10.90	
(S)-(+)-carvone	37.64	38.20	38.70	38.10	38.37	38.85	9.35	9.52	9.61	9.70	9.72	9.77	
Carvacrol													
DL-citronellol	7.45	8.04	8.63	9.04	9.63	10.02							
Eucalyptol	163.23	160.88	155.07	148.60	148.80	144.22	32.35	32.02	31.68	31.14	30.76	30.25	
Eugenol													
Geraniol	5.26	5.84	6.44	6.92	7.51	7.94							
L(-)-menthol	9.68	10.44	11.17	11.90	12.19	13.02	4.56	4.85	5.00	5.27	5.43	5.62	
Linalool	85.73	118.63	161.79	213.13	282.51	364.59	39.49	53.93	72.09	95.84	127.35	162.26	
Thymol													
$\alpha$ -pinene oxide	88.60	91.21	94.04	99.10	101.31	104.70	7.94	8.61	9.26	9.95	10.67	11.49	

**Table S2.** Activity coefficients at infinite dilution of terpenes and terpenoids in ILs, at different temperatures. <sup>a</sup> (cont)

Solutes <i>T/K</i>	[C <sub>4</sub> mim][(CH <sub>3</sub> ) <sub>2</sub> PO <sub>4</sub> ] <sup>d</sup>						[C <sub>4</sub> mim][CF <sub>3</sub> SO <sub>3</sub> ] <sup>e</sup>					
	398.15	408.15	418.15	428.15	438.15	448.15	398.15	408.15	418.15	428.15	438.15	448.15
$\alpha$ -pinene	29.54	28.98	28.43	28.04	27.81	27.72	25.73	25.11	24.37	23.84	23.20	22.76
$\beta$ -pinene	23.09	22.79	22.47	22.28	22.14	22.06	19.40	18.92	18.63	18.25	17.86	17.58
(-)-borneol							2.80	2.45	2.12	1.86	1.66	1.41
(-)-Isopulegol							3.84	3.92	3.95	4.01	4.09	
(-)-menthone	12.41	12.44	12.52	12.67	12.86	13.13	5.87	5.96	6.06	6.17	6.28	6.47
(1R)-(-)-fenchone	8.94	8.91	8.86	8.89	8.87	8.90	4.16	4.10	4.15	4.19	4.22	4.25
(1R)-(+)-camphor	7.93	7.96	7.98	8.02	8.05	8.11	3.71	3.78	3.86	3.93	4.03	4.09
(S)-(+)-carvone	7.17	7.26	7.35	7.46	7.55	7.67	4.13	4.21	4.28	4.34	4.40	4.44
Carvacrol								0.60	0.66	0.73	0.81	0.86
DL-citronellol							5.13	5.24	5.29	5.39	5.55	
Eucalyptol	19.04	18.81	18.91	18.88	18.70	18.91	12.34	12.31	12.33	12.34	12.38	12.32
Eugenol								1.25	1.34	1.45	1.55	1.59
Geraniol							4.09	4.29	4.45	4.65	4.83	
L(-)-menthol							5.50	5.62	5.66	5.74	5.84	
Linalool	9.96	14.26	20.00	27.73	37.18	52.02	48.52	63.49	81.46	104.32	132.40	158.94
Thymol								0.60	0.67	0.75	0.82	0.88
$\alpha$ -pinene oxide	11.40	11.95	12.60	13.24	13.90	14.75	6.18	6.49	6.86	7.24	7.64	7.90

<sup>a</sup>Standard uncertainties are:  $u(\gamma_{13}^{\infty}) = 3\%$  and  $u(T) = 0.02\text{ K}$ . <sup>b</sup>Packing: 52.1 %,  $n_3 = 17.02\text{ mmol}$ . <sup>c</sup>Packing: 49.8 %,  $n_3 = 11.48\text{ mmol}$ . <sup>d</sup>Packing: 47.3 %,  $n_3 = 9.39\text{ mmol}$ . <sup>e</sup>Packing: 49.1 %,  $n_3 = 8.75\text{ mmol}$ .

**Table S3.** Infinite dilution partial molar excess enthalpies  $\overline{H}_m^{E,\infty}$  / kJ·mol<sup>-1</sup>, excess Gibbs free energies  $\overline{G}_m^{E,\infty}$  / kJ·mol<sup>-1</sup>, and entropies  $T_{ref} \overline{S}_m^{E,\infty}$  / kJ·mol<sup>-1</sup>, for terpenes, terpenoids and water in the ILs investigated in this work, at 408.15 K.<sup>a</sup>

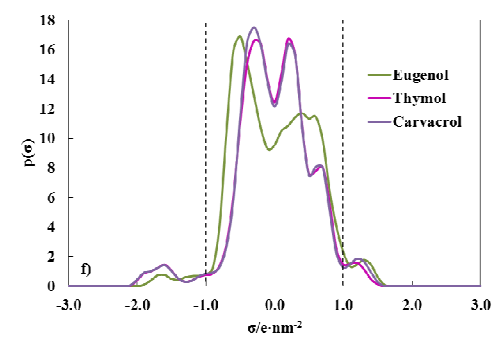
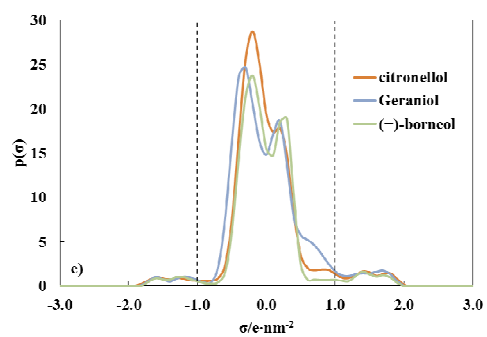
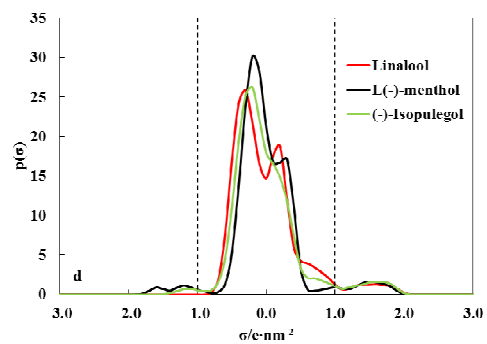
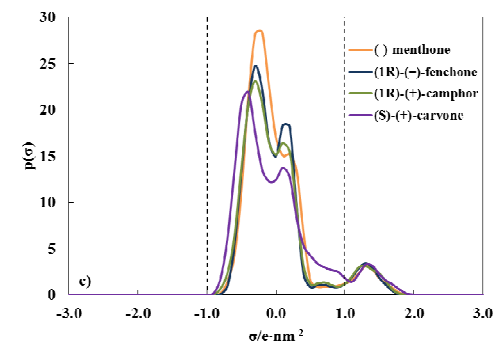
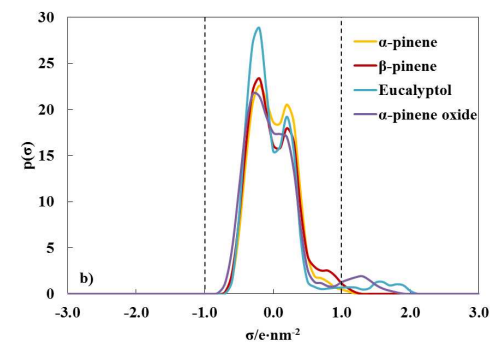
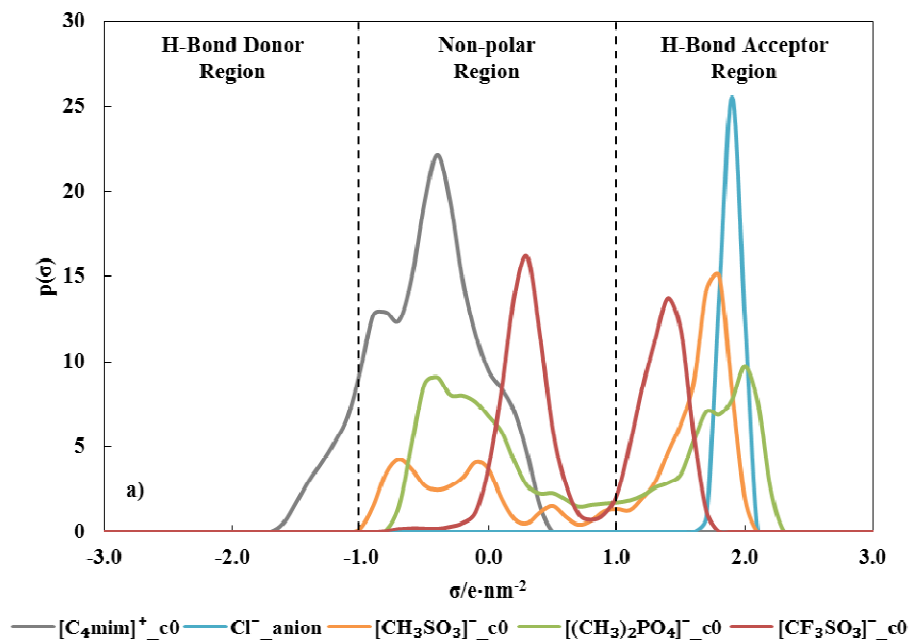
Solutes	[C <sub>4</sub> mim]Cl			[C <sub>4</sub> mim][CH <sub>3</sub> SO <sub>3</sub> ]			[C <sub>4</sub> mim][(CH <sub>3</sub> ) <sub>2</sub> PO <sub>4</sub> ]			[C <sub>4</sub> mim][CF <sub>3</sub> SO <sub>3</sub> ]		
	$\overline{H}_m^{E,\infty}$	$\overline{G}_m^{E,\infty}$	$T_{ref} \overline{S}_m^{E,\infty}$	$\overline{H}_m^{E,\infty}$	$\overline{G}_m^{E,\infty}$	$T_{ref} \overline{S}_m^{E,\infty}$	$\overline{H}_m^{E,\infty}$	$\overline{G}_m^{E,\infty}$	$T_{ref} \overline{S}_m^{E,\infty}$	$\overline{H}_m^{E,\infty}$	$\overline{G}_m^{E,\infty}$	$T_{ref} \overline{S}_m^{E,\infty}$
α-pinene	8.41	19.11	-10.70	4.54	13.77	-9.24	1.94	11.42	-9.48	3.70	10.94	-7.24
β-pinene	5.20	18.01	-12.81	2.62	12.72	-10.10	1.38	10.61	-9.23	2.91	9.98	-7.07
(-)-borneol	13.18	4.08	9.10							20.00	3.04	16.96
(-)-isopulegol	-7.75	7.23	-14.98	-5.20	4.69	-9.89				-1.35	4.64	-5.99
(-)-menthone	0.00	15.33	-15.33	0.00	9.70	-9.70	-1.64	8.56	-10.19	-2.78	6.06	-8.84
(1R)-(-)-fenchone	3.20	14.01	-10.81	1.34	8.58	-7.24	0.00	7.42	-7.42	0.00	4.79	-4.79
(R)-(+)-camphor	0.00	13.37	-13.37	0.00	8.07	-8.07	-0.64	7.04	-7.68	-2.93	4.52	-7.45
(S)-(+)-carvone	0.00	12.36	-12.36	-1.25	7.65	-8.90	-1.97	6.73	-8.70	-2.18	4.88	-7.06
Carvacrol										-14.14	-1.74	-12.40
DL-citronellol	-8.79	7.07	-15.86							-2.13	5.62	-7.75
Eucalyptol	3.80	17.24	-13.44	2.00	11.76	-9.76	0.00	9.96	-9.96	0.00	8.52	-8.52
Eugenol										-9.47	0.77	-10.24
Geraniol	-12.26	5.99	-18.25							-5.05	4.94	-10.00
L(-)-menthol	-8.54	7.96	-16.50	-6.07	5.36	-11.43				-1.20	5.86	-7.06
Linalool	-42.92	16.21	-59.13	-42.11	13.53	-55.64	-48.62	9.02	-57.64	-35.58	14.09	-49.67
Thymol										-14.70	-1.72	-12.97
α-pinene oxide	-5.09	15.32	-20.41	-10.87	7.31	-18.18	-7.58	8.42	-16.00	-7.51	6.35	-13.86

<sup>a</sup>Standard uncertainties:  $u(\overline{H}_m^{E,\infty}) = \pm 0.5$  kJ·mol<sup>-1</sup>;  $u(\overline{G}_m^{E,\infty}) = \pm 0.5$  kJ·mol<sup>-1</sup>;  $u(T_{ref} \overline{S}_m^{E,\infty}) = \pm 0.05$  kJ·mol<sup>-1</sup>.

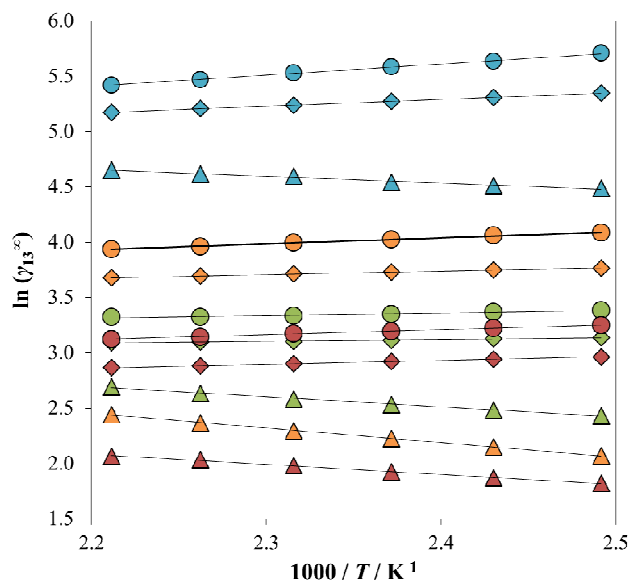
**Table S4.** Gas–liquid partition coefficients,  $K_L$ , for terpenes, terpenoids and water in ILs, at different temperatures.<sup>a</sup>

Solutes	[C <sub>4</sub> mim]Cl					[C <sub>4</sub> mim][CH <sub>3</sub> SO <sub>3</sub> ]					[C <sub>4</sub> mim][(CH <sub>3</sub> ) <sub>2</sub> PO <sub>4</sub> ]					[C <sub>4</sub> mim][CF <sub>3</sub> SO <sub>3</sub> ]								
	T / K	398.15	408.15	418.15	428.15	438.15	448.15	398.15	408.15	418.15	428.15	438.15	448.15	398.15	408.15	418.15	428.15	438.15	448.15	398.15	408.15	418.15	428.15	438.15
$\alpha$ -pinene	1.50	1.23	1.00	0.83	0.71	0.60	6.12	4.78	3.82	3.11	2.55	2.12	10.81	8.38	6.61	5.27	4.23	3.43	12.58	9.80	7.81	6.26	5.12	4.22
$\beta$ -pinene	2.83	2.23	1.77	1.43	1.16	0.97	11.08	8.50	6.64	5.26	4.23	3.45	18.19	13.89	10.80	8.48	6.74	5.42	21.96	16.95	13.18	10.47	8.44	6.86
(-)-borneol	785.84	493.04	318.50	210.54	147.30	104.85													721.70	477.97	328.00	227.97	160.66	120.92
(-)-isopulegol	301.22	193.18	127.16	87.57	60.45	43.43	503.45	327.95	221.51	152.85	108.90	78.73							441.15	295.91	205.79	144.85	103.77	
(-)-menthone	25.93	18.36	13.47	10.06	7.67	6.03	109.14	77.31	56.45	42.16	32.01	24.66	133.68	95.17	68.98	50.76	37.91	28.66	286.68	201.15	144.21	105.37	78.39	58.65
(1R)-(-)-fenchone	20.49	15.15	11.31	8.75	6.88	5.32	83.16	60.19	44.97	33.95	26.08	20.37	102.66	74.40	55.03	41.12	31.37	24.17	223.61	163.73	119.02	88.16	66.51	51.02
(R)-(+)-camphor	42.39	30.00	21.98	16.39	12.46	9.72	161.32	115.00	84.01	62.51	47.41	36.52	191.09	136.64	99.87	74.21	56.13	43.03	414.57	291.12	208.69	153.06	113.35	86.09
(S)-(+)-carvone	134.12	91.00	63.12	45.91	33.23	24.34	433.81	293.06	203.87	144.70	105.21	77.48	496.30	337.15	233.97	165.02	118.77	86.61	874.47	589.10	406.25	286.47	205.67	150.81
Carvacrol																				6714.15	4107.89	2576.97	1645.91	1110.90
DL-citronellol	841.24	507.87	316.87	207.26	136.49	93.85													873.79	556.69	367.87	247.18	167.95	
Eucalyptol	4.97	3.74	2.93	2.35	1.83	1.50	20.14	15.09	11.53	9.01	7.11	5.72	30.03	22.55	16.94	13.03	10.26	8.03	46.97	34.89	26.29	20.15	15.65	12.43
Eugenol																				5011.76	3157.99	2020.42	1324.07	924.91
Geraniol	1416.48	845.52	519.65	334.42	217.06														1300.25	822.09	536.47	353.62	239.69	
L(-)-menthol	399.55	249.86	160.94	106.33	74.34	50.84	680.85	432.01	288.46	192.58	133.78	94.33							502.93	331.35	226.39	156.75	110.18	
Linalool	244.81	153.37	98.79	66.64	45.13	31.67	426.84	270.88	177.93	118.87	80.28	57.04	1485.84	898.76	562.53	360.36	241.14	156.00	309.23	204.54	139.79	96.84	68.37	51.50
Thymol																				5323.24	3270.67	2061.33	1337.80	908.40
$\alpha$ -pinene oxide	15.81	11.70	8.81	6.61	5.21	4.11	141.77	99.48	71.78	52.85	39.59	29.97	86.62	62.91	46.30	34.81	26.66	20.47	162.01	117.24	86.09	64.34	48.95	38.55

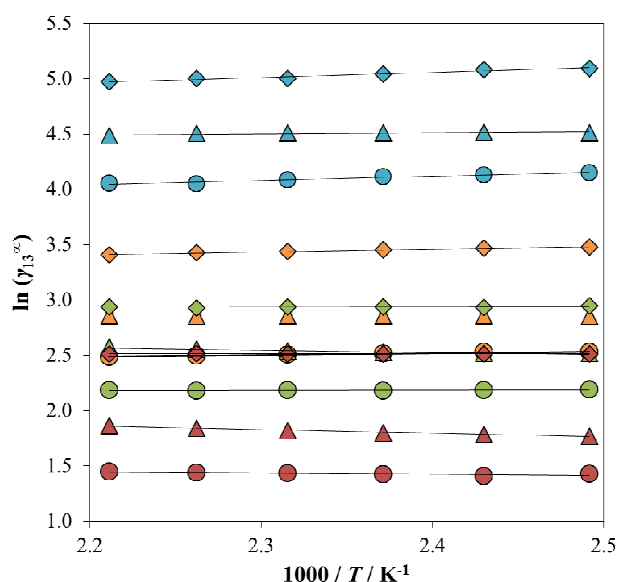
<sup>a</sup>Standard uncertainties:  $u(K_L) < 3\%$  and  $u(T) = 0.02$  K.



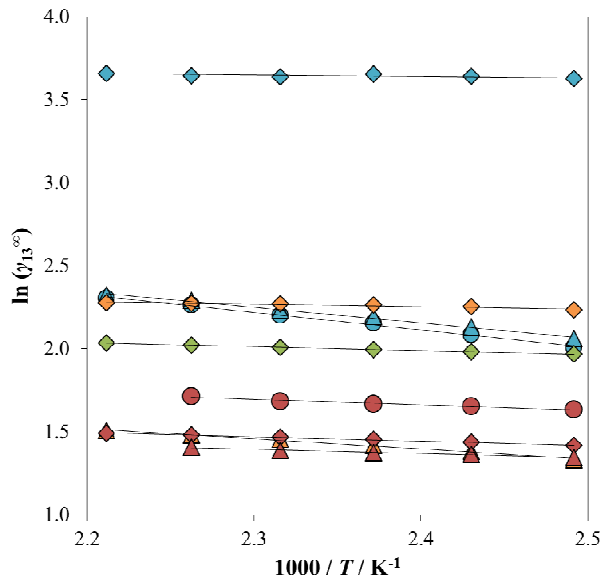
**Figure S1.** Sigma profiles of: a) ionic liquids; b) hydrocarbons and ethers; c) ketones; d), e) and f) alcohols, computed by COSMO-RS.



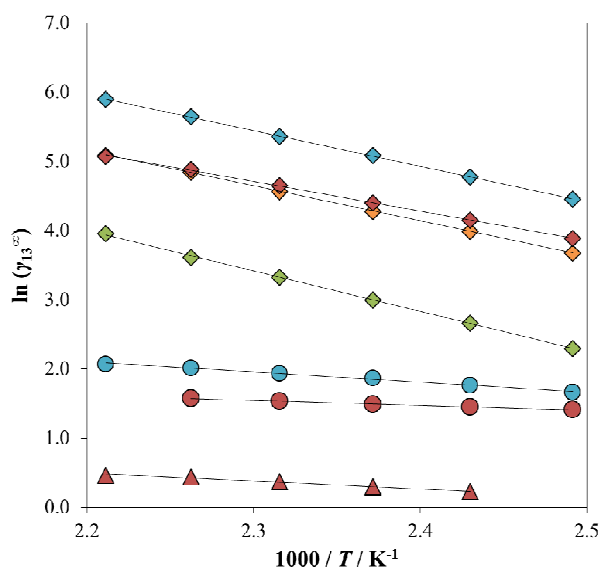
○  $\alpha$ -pinene; ◇  $\beta$ -pinene; △  $\alpha$ -pinene oxide



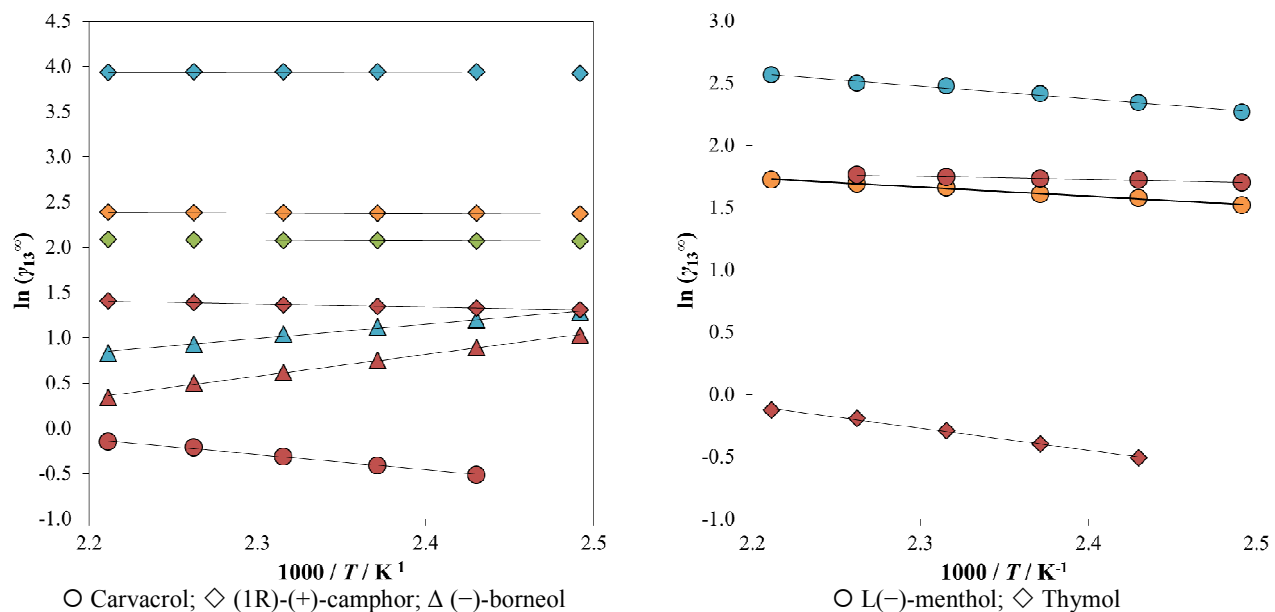
○ (1R)-(-)-fenchone; ◇ Eucalyptol; △ (-)-menthone



○ DL-citronellol; ◇ (S)-(+)-carvone; △ (-)-isopulegol

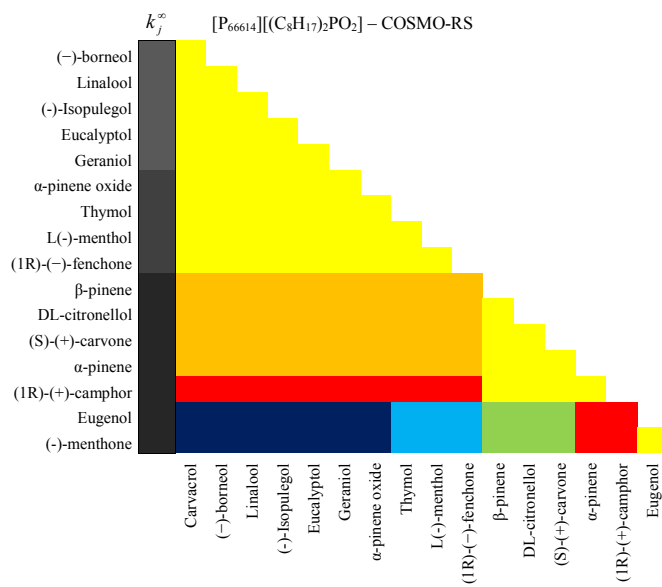
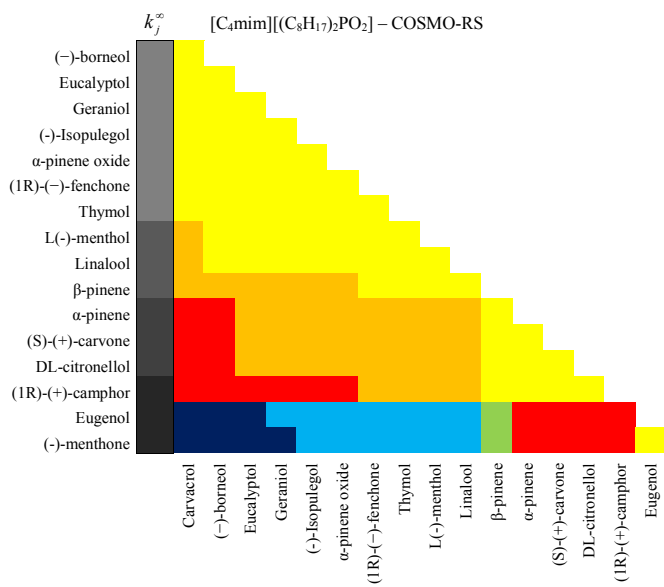
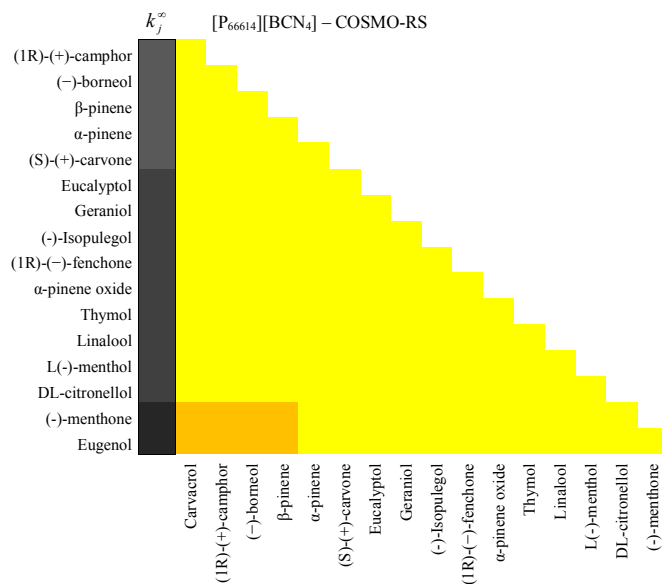
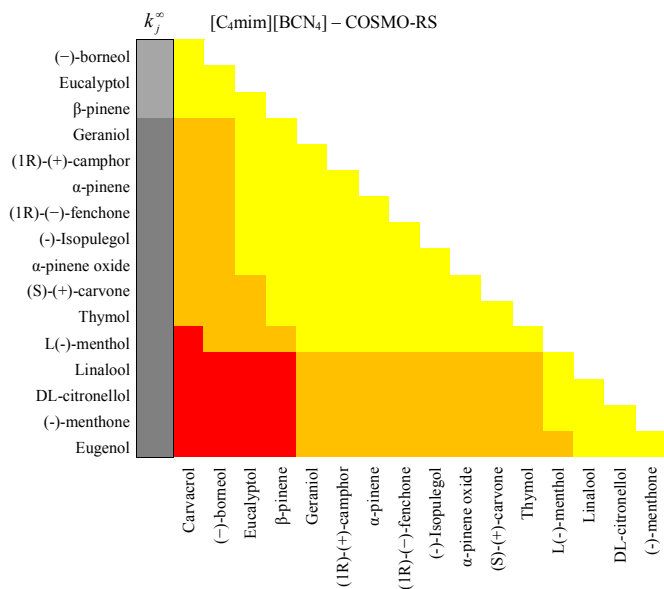


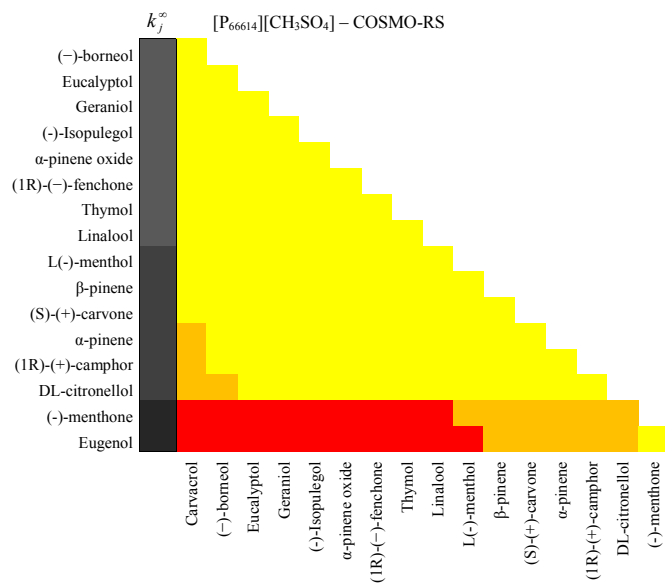
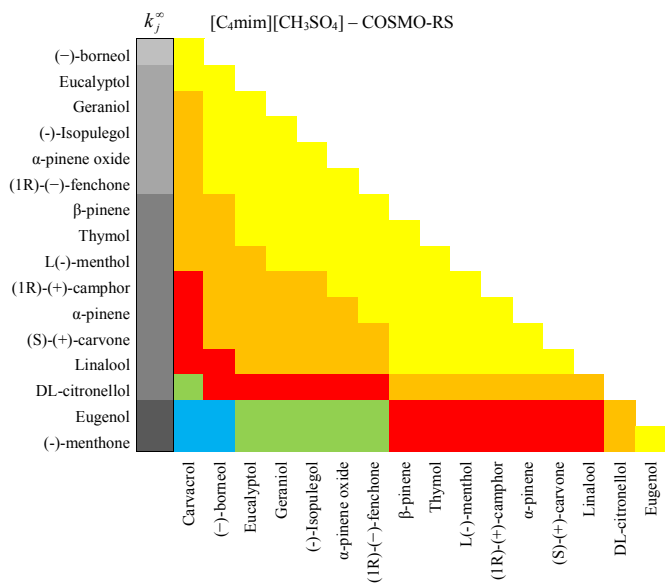
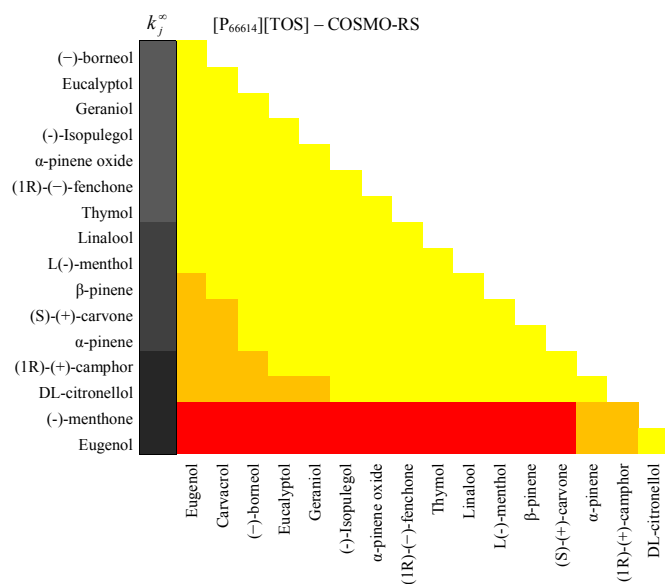
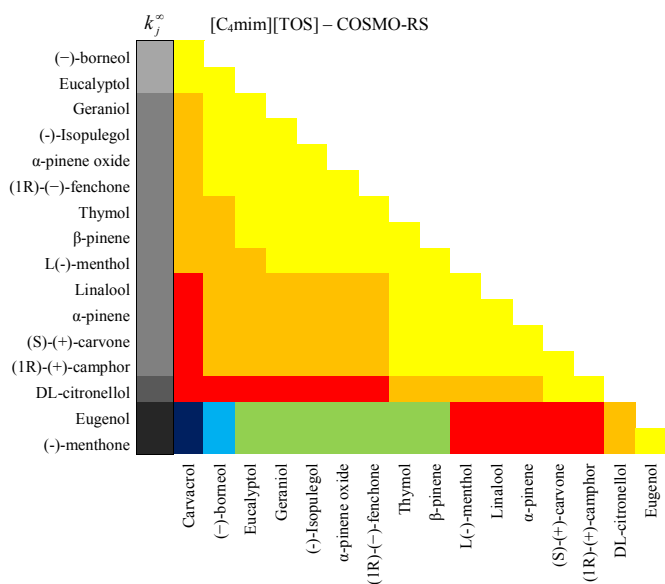
○ Geraniol; ◇ Linalool; △ Eugenol

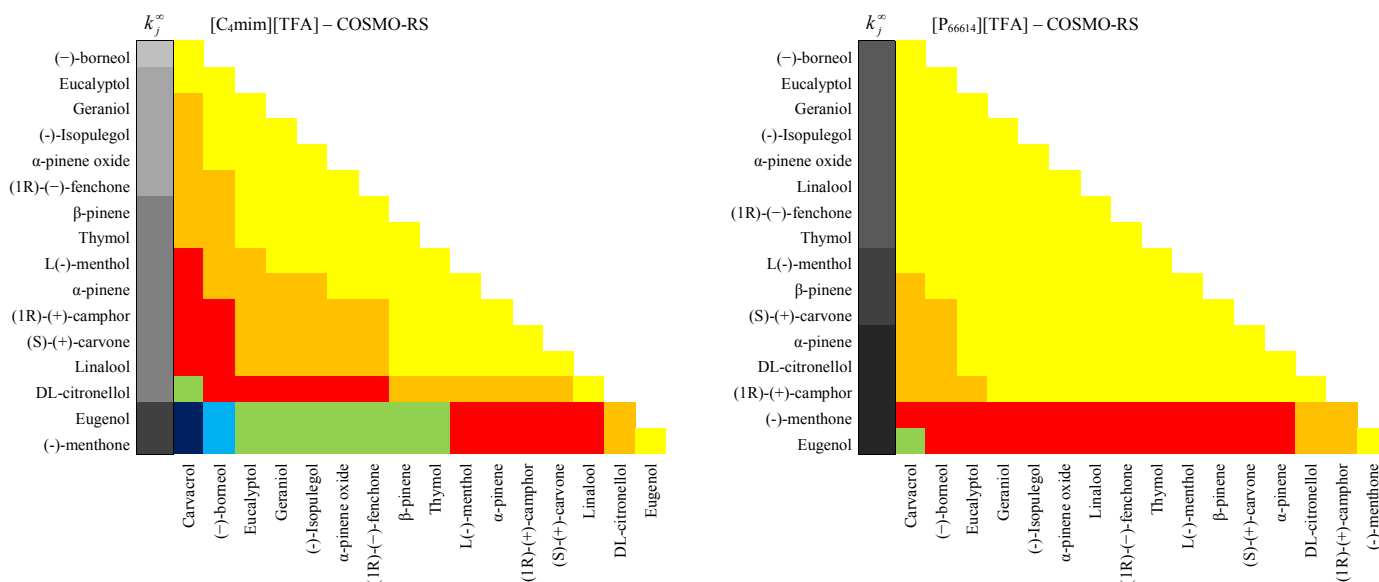


**Figure S2.** Experimental natural logarithm of activity coefficients at infinite dilution as a function of the inverse absolute temperature for all the studied solutes in:  $\bullet$ , [C<sub>4</sub>mim]Cl;  $\bullet$ , [C<sub>4</sub>mim][CH<sub>3</sub>SO<sub>3</sub>];  $\bullet$ , [C<sub>4</sub>mim][((CH<sub>3</sub>)<sub>2</sub>PO<sub>4</sub>) and  $\bullet$ , [C<sub>4</sub>mim][CF<sub>3</sub>SO<sub>3</sub>].









**Figure S3.**  $S_{ij}^\infty$  and  $k_j^\infty$  of all solutes at 408.15 K in selected ionic liquids, computed by COSMO-RS. Cations: [C<sub>4</sub>mim]<sup>+</sup>, 1-butyl-3-methyl-imidazolium; [P<sub>66614</sub>]<sup>+</sup>, trihexyltetradecylphosphonium. Anions: [BCN<sub>4</sub>]<sup>-</sup>, tetracyanoborate; [(C<sub>8</sub>H<sub>17</sub>)<sub>2</sub>PO<sub>2</sub>]<sup>-</sup>, bis(2,4,4-trimethylpentyl)phosphinate; [TOS]<sup>-</sup>, tosylate; [CH<sub>3</sub>SO<sub>4</sub>]<sup>-</sup>, methylsulfate; and [TFA]<sup>-</sup>, trifluoroacetate. Color code: Selectivities, ■ [1-2]; ■ [2-4]; ■ [4-10]; ■ [10-20]; ■ [20-30]; and ■ >30; Capacities, ■ <0.01; ■ [0.01-0.05]; ■ [0.05-0.1]; ■ [0.1-0.2]; ■ [0.2-1]; ■ [1-2]; ■ [2-5]; and ■ > 5.

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