

1 Valorization of expired energy drinks by
2 designed and integrated ionic-liquid-based
3 aqueous biphasic systems

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17 **KEYWORDS.** Food industrial wastes; Circular economy; Energy drinks, Valorization;
18 Recovery; Ionic liquids.

19 **ABSTRACT**

20 Expired energy drinks are rich in bioactive added-value compounds that can be recovered
21 and reused in order to valorize food waste within a circular economy perspective.
22 However, to accomplish such requirements it is necessary to develop sustainable
23 extraction and recovery processes, which must comprise a decrease in the number of steps
24 required or by developing integrated strategies. In this work, novel aqueous biphasic
25 systems (ABS) composed of ionic liquids (ILs) and a biocompatible polymer
26 polypropylene glycol (400 g.mol⁻¹, PPG 400) were studied for the simultaneous
27 extraction and recovery of three added-value compounds, namely caffeine, taurine and
28 niacin, from expired energy drinks. ILs were designed and synthesized in order to have
29 similar anions to the target compounds, thus allowing enhanced selectivity and biological
30 activity, while avoiding an extra step of separation of these high-value compounds from
31 the IL-rich phase. To this end, cholinium-based ILs comprising the anions lactate,
32 pyruvate, taurate and nicotinate were synthesized and their cytotoxicity and ecotoxicity
33 credentials evaluated. Overall, taurine and niacin are majorly enriched in the IL-rich
34 phase, while caffeine preferentially migrates in the majority of the cases towards the PPG-
35 rich phase. However, caffeine also partitions to the IL-rich phase in the ABS formed by
36 cholinium pyruvate and cholinium nicotinate. The ABS formed by cholinium nicotinate
37 and PPG 400 is the best system identified, allowing the almost complete recovery
38 (recovery efficiencies >82%) of all target compounds into the IL-rich phase in one-step.
39 Furthermore, cholinium nicotinate exhibits marginal cytotoxic potential and is harmless
40 from an ecotoxicological point of view. This system is thus a promising platform to
41 simultaneously extract, recover and reuse added-value compounds from expired energy
42 drinks without the need of removing the IL or recovering the target compounds from the
43 IL-rich phase, thus contributing to a sustainable and circular food economy.

44 INTRODUCTION

45 In developed countries an increasing amount of food is not consumed and ends up as
46 waste along the food value chain, creating a relevant economic and environmental
47 problem.¹ As disclosed by the Food and Agriculture Organization of the United Nations
48 (FAO), one third of the food produced worldwide for human consumption (1.3 billion
49 tonnes per year) is lost or wasted.² In the European Union, for instance, food waste is
50 projected to rise to 126 million tons by 2020.¹ Currently, food waste constitutes a relevant
51 concern, being linked to negative economic, societal and environmental impacts.³
52 Accordingly, the valorization of food waste is a priority measure to reduce the carbon
53 footprint of the food production chain⁴ and to improve economy as the residues generated
54 may contain high-value compounds.⁵ In the framework of circular economy, these
55 evidences reinforce the need on the development of cost-effective and sustainable
56 technologies to recover added-value compounds from food waste.

57 Among food waste, energy drinks, particularly rich in stimulants and additives, play a
58 significant role. These beverages contain high levels of caffeine (up to 500 mg *per* bottle)
59 and are usually supplemented with taurine, glucuronolactone, and complex B vitamins.⁶
60 Most of these high-value compounds maintain their biological activity, even after the
61 expiration dates of energy drinks. In addition to the environmental concerns generated by
62 this type of drinks, their discharge indirectly has an economic impact by increasing their
63 waste management and production costs. Thus, the recovery and reuse of added-value
64 and bioactive compounds from discharged energy drinks has a relevant environmental
65 and economic influence on this market sector that registered global sales over €38 billion
66 in 2015, being expected to reach €53.4 billion in 2020.⁷

67 Several methods, including liquid-liquid extraction,⁸ nanofiltration⁹ and solid-phase
68 extraction¹⁰ have been reported for the recovery of target compounds from diet samples

69 and beverages. In addition to the extraction step, separation and purification processes are
70 needed, which may comprise numerous drawbacks, including high energy and chemicals
71 consumption.^{11, 12} Furthermore, most of these methods are time consuming, labour
72 intensive and use volatile organic solvents, contributing to a relevant environmental
73 impact. Overall, cost-efficient and sustainable techniques able to provide high recovery
74 yields and purity levels of valuable compounds recovered from food waste, ideally
75 combining or integrating several steps, must be developed to meet the current society and
76 environmental standards.

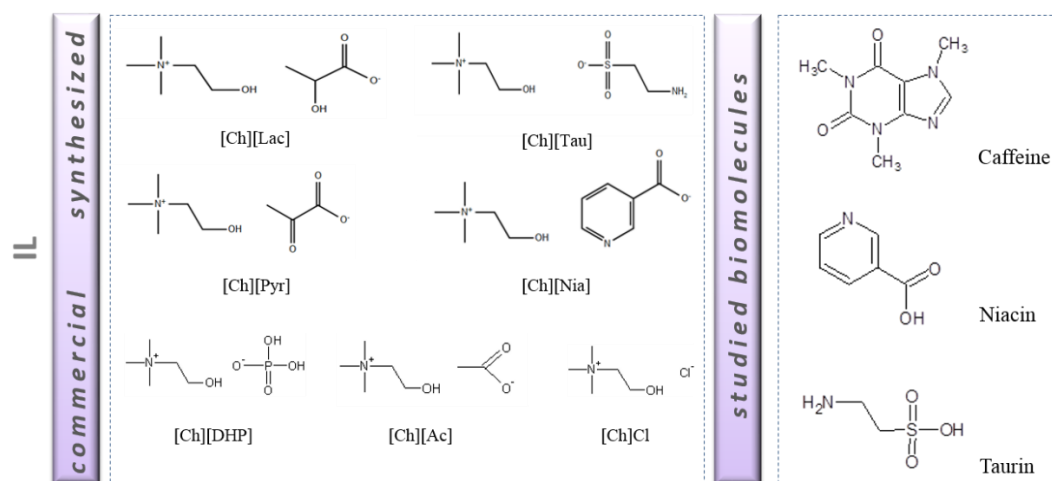
77 Aqueous biphasic systems (ABS) are downstream processing alternatives acting by
78 liquid-liquid extraction, allowing to recover target products from complex samples.¹³
79 Accordingly, this type of systems can be applied both in the extraction and purification
80 steps of high-value compounds from food waste.¹⁴ Moreover, if properly designed, ABS
81 may be biocompatible and of low cost.^{15, 16} Typical ABS consist of two immiscible
82 aqueous-rich phases based on polymer/polymer, polymer/salt or salt/salt combinations.
83 In order to improve their separation performance, ABS formed by ionic liquids (ILs) have
84 been extensively investigated.¹⁵ Besides other relevant properties, their fine-tuning by
85 combining adequate IL cations and anions is one of the most significant.^{15, 17, 18}

86 ILs are able to form ABS in presence of salts, amino acids, carbohydrates or polymers,
87 and have been successfully used in the extraction of phenolic acids, alkaloids, amino
88 acids, proteins, among others.¹⁹⁻²¹ However, several concerns have been raised with the
89 most studied ILs in this field, mainly imidazolium-based.^{22, 23} This trend is however
90 changing, with novel classes of ILs being proposed for the creation of ABS.^{19, 21} Among
91 these, cholinium-based ILs have been the main target since the IL cation is an important
92 micronutrient source belonging to the B-complex vitamins, which may thus overcome the
93 main drawback on the use of ILs in the food industry²⁴. Cholinium chloride ([Ch]Cl) is

94 currently classified as a safe substance by the U.S. Food and Drug Administration
95 (FDA).²⁵ Previous works reported the synthesis of cholinium-based ILs alongside with
96 their toxicological and biodegradation potential, showing that when combined with
97 appropriate anions, these ILs exhibit low toxicity and high biodegradability.²⁶
98 ABS based on cholinium-based ILs were successfully used in the extraction of
99 flavonoids, polysaccharides, amino acids, proteins and enzymes from aqueous solutions
100 and from complex matrices.^{19, 27-29} Some publications can be found in the literature
101 regarding the use of IL-based ABS in the valorization of food waste,^{25, 27, 30, 31} yet, the
102 majority of these works focused on ABS formed by imidazolium-based ILs and salts, thus
103 compromising their green credentials, and none envisioned the use of ILs with similar
104 biological features to enhance the biological properties of the recovered compounds,
105 while avoiding the use of an additional step to recover the target compounds from the IL-
106 rich phase. The non-volatile nature of ILs, which is valuable when addressing it from an
107 environmental perspective, is indeed a major drawback when attempting the recovery of
108 target compounds from the IL-rich phase since a simple distillation step cannot be
109 applied. Therefore, and although scarcely considered, the recovery of the target
110 compounds from IL-rich phases has been achieved by the addition of anti-solvents, back-
111 extraction steps with organic solvents or by the use of solid-phase extraction.^{32, 33}
112 Aiming at developing a sustainable and cost-effective process for the recovery of added-
113 value compounds (caffeine, taurine and niacin) from expired energy drinks, we here
114 demonstrate the potential of ABS formed by cholinium-based ILs (4 synthesized ILs and
115 3 commercial ILs for comparison purposes) and polypropylene glycol with a molecular
116 weight of 400 g.mol⁻¹ (PPG 400) to directly extract the target compounds from the real
117 samples. By being extracted to the IL-rich phase, and by using ILs with similar biological
118 features, the additional separation step to recover the target compounds from the IL-rich

119 phase can be avoided, and may result in an integrated process. The chemical structures
 120 and abbreviations of the investigated ILs are depicted in Figure 1.
 121 The synthesized ILs comprise anions derived from natural sources, such as from plant
 122 natural acids (lactate and pyruvate), amino acids (taurate) and vitamins (nicotinate).
 123 These ILs were designed taking into account the target compounds to recover from
 124 expired energy drinks, which could have their biological properties enhanced if combined
 125 with IL anions with similar properties. Bearing in mind the potential reuse of the
 126 recovered compounds combined with adequate ILs, the ILs cytotoxicity towards human
 127 intestinal cell lines and their ecotoxicity by the microtox assay were evaluated. The
 128 recovery performance of the investigated ABS for caffeine (alkaloid), taurine (amino
 129 acid) and niacin (vitamin B3) from expired energy drinks was finally addressed. The
 130 target biomolecules, whose chemical structures are given in Figure 1, are important in the
 131 maintenance of the body homeostasis and are widely used by the food, cosmetic and
 132 pharmaceutical industries.³⁴⁻³⁹

133



134

135 **Figure 1.** Chemical structures of the investigated ILs and added-value compounds.

136

137

138 **EXPERIMENTAL SECTION**

139 **Materials.** Poly(propylene glycol) with an average molecular weight of $400 \text{ g}\cdot\text{mol}^{-1}$
140 (PPG400), cholinium hydroxide ([Ch][OH], 46 wt% in water), taurine (purity $\geq 99\%$),
141 lactic acid (purity $\geq 98\%$), pyruvic acid (purity $\geq 98\%$), nicotinic acid (purity $\geq 99.5\%$),
142 2,4-dinitrofluoro benzene (DNFB purity $\geq 99\%$) and dimethyl sulfoxide (DMSO; purity
143 $>99.0\%$) were purchased from Sigma Aldrich (St. Louis, MO, USA). Methanol and
144 acetonitrile (HPLC grade, purity $>99.9\%$) were obtained from Fisher Chemical (Fisher
145 Scientific, USA). Commercial ILS, namely cholinium acetate ([Ch][Ac], $>99 \text{ wt}\%$) and
146 cholinium dihydrogen phosphate ([Ch][DHP], $>98 \text{ wt}\%$), were acquired from Iolitec,
147 while cholinium chloride ([Ch]Cl, $>98 \text{ wt}\%$) was purchased from Acros Organic.

148 The cell culture medium (Dulbecco's Modified Eagles's Medium – high glucose (HG))
149 used in the cytotoxicity assays was obtained from Sigma, Fetal Bovine Serum (FBS) from
150 Merck Millipore and 3-(4,5-dimethylthiazol-2-yl)-2,5-diphenyltetrazolium bromide
151 (MTT) (purity 98%) from ACROS Organics. All chemicals for ecotoxicity assays were
152 purchased from Ambifirst.

153 The sample of energy drink (sugar free Red Bull®) was acquired from a local market in
154 Aveiro (Portugal); it was used in all experiments with one month after the expiration date.
155 According to the product label it contains caffeine, taurine, B-group vitamins (B3, B5,
156 B6 and B12), aspartame, acesulfame K and water.

157 **ILs Synthesis.** Synthesis of cholinium lactate ([Ch][Lac])⁴⁰, cholinium nicotinate
158 ([Ch][Nia])⁴¹ and cholinium taurate ([Ch][Tau])⁴², were performed according to
159 previously described protocols. Cholinium pyruvate ([Ch][Pyr]) was synthesized in this
160 work for the first time by acid-base titration. The potentiometric acid-base titrations were
161 performed by the slow addition of an aqueous solution of [Ch][OH] (at $1.7524 \text{ mol}\cdot\text{L}^{-1}$)
162 to lactic, pyruvic, nicotinic and 2-aminoethanesulfonic acids. [Ch][OH] was added in

163 small excess and then back titrated by adding the acid solution until the desired inflection
164 point is obtained (pH values for [Ch][Lac] = 9.25, [Ch][Pyr] = 8.20, [Ch][Nia] = 7.95 and
165 [Ch][Tau] = 9.02). Excess water was first removed from the synthesized ILs at 70°C using
166 a rotational evaporator, and then under vacuum until constant weight was achieved. ILs
167 were stored with P₂O₅ under vacuum for the following 72 h. The water content in the ILs
168 was determined by Karl-Fisher titration and found to be ≤ 200 ppm in all ILs. The
169 chemical structures and purities of the synthesized ILs, [Ch][Lac] (> 98 wt%), [Ch][Pyr]
170 (>96 wt%), [Ch][Nia] (>99 wt%) and [Ch][Tau] (>99 wt%), were confirmed by ¹H and
171 ¹³C Nuclear Magnetic Resonance (NMR) and Fourier-transform infrared spectroscopy
172 (FTIR) spectroscopy (Figures S1–S6 in the Supporting Information). NMR spectra were
173 recorded in D₂O at 25°C on a Bruker Advance III 400 MHz spectrometer.
174 Tetramethylsilane was used as internal standard. FTIR spectra were recorded from (4000
175 to 650) cm⁻¹ using a Thermo-Nicolet Nexus 670 spectrometer fitted with a Universal ATR
176 Sampling Accessory. The chemical structures of the investigated ILs are given in Figure
177 1.

178 **ILs cytotoxicity and ecotoxicity.** The cytotoxicity of the synthesized ILs ([Ch][Lac],
179 [Ch][Nia], [Ch][Pyr], [Ch][Tau]) alongside with the commercial ILs [Ch][Ace], [Ch]Cl
180 and [Ch][DHP] was addressed in the human colon epithelial cell line (Caco-2). A stock
181 solution of each IL was prepared in saline aqueous solutions and the test solutions were
182 obtained by successive dilutions of the stock in culture medium, obtaining the final
183 concentrations of 0.1, 1.0, 10, 30, 60, 90 g.L⁻¹ of each IL. The epithelial human colon cell
184 line (Caco-2) was grown in high glucose Dulbecco's modified Eagle's medium (DMEM-
185 HG) containing 10% (v/v) fetal bovine serum (FBS), 100 units penicillin, and 50 µg.mL⁻¹
186 streptomycin in a humidified atmosphere of 5% CO₂ at 37°C. Cells were plated on
187 polystyrene cell culture dishes at a density of 1x10⁴ cells *per* well in 96 well culture plates.

188 After 16 h, cells were treated with the different concentrations of the target ILs for 24h.
189 Cytotoxicity was evaluated using the 3-(4,5-dimethylthiazol-2-yl)-2,5-
190 diphenyltetrazolium bromide (MTT) assay. This assay is based on the ability of viable
191 cells to convert MTT into a water-insoluble precipitate. Caco-2 cells were incubated with
192 0.5 mg.dm⁻³ of MTT in medium overnight at 37 °C. The precipitate was then dissolved
193 in 10% (w/v) sodium dodecyl sulfate (SDS), and colorimetrically quantified (at 570 nm)
194 using a microplate spectrophotometer. Each concentration was tested in five replicates of
195 three independent experiments ($n=3$), except for [Ch]Cl for which the values correspond
196 to five replicates of two independent experiments ($n=2$). In all experiments, a negative
197 control corresponding to untreated cells was always included.

198 The dose response curves and median effective concentration (EC₅₀) calculations were
199 performed using the GraphPad PRISM Software (version 8.0.1). The EC₅₀ corresponds
200 to the concentration of IL for which 50% of the cells are viable. Cell viability results are
201 expressed as percentage of the control (i.e. unexposed cells).

202 The ecotoxicity of the synthesized ILs was evaluated using the Standard Microtox liquid-
203 phase assays. This test evaluates the inhibition of the luminescence of the marine bacteria
204 *Vibrio fischeri* and was performed using a range of diluted aqueous solutions (from 0 to
205 81.9%) of IL, where 100% of the compound corresponds to a known concentration of a
206 stock solution (ca. 10 g.L⁻¹). After 5, 15, and 30 min of exposure to IL, the light output of
207 the luminescent bacteria was determined and compared with the light output of a blank
208 control sample. The toxicity was evaluated on the basis of the percentage decrease in the
209 bacteria luminescence relative to the blank control. The final output of this test is the EC₅₀
210 parameter, which represents the effective concentration of a given IL that produces 50%
211 of inhibition of light emission. Analyses were performed with the MicrotoxOmni™
212 Software version 4.3.0.1.

213

214 **ABS phase diagrams and recovery studies.** The phase diagrams of the ABS composed
215 of each IL, PPG 400 and water were determined through the cloud point titration method
216 at (25 ± 1) °C and at atmospheric pressure, as previously described.⁴³⁻⁴⁵ Details regarding
217 phase diagram determination are given in the Supporting Information. Initial tests to
218 address the real samples effect in the binodal curves was carried out, with no significant
219 differences (within the experimental error) obtained between the phase diagrams
220 determined with water or with energy drink samples. This fact is due to the low amount
221 of additives present when compared to the amounts of IL and PPG 400 required to create
222 ABS.

223 After addressing the ABS phase diagrams and compositions required to create two-phase
224 systems, their recovery capability for the three biomolecules from expired drinks was
225 evaluated at two mixture compositions: (15 wt% IL + 40 wt% PPG400 + 45 wt% expired
226 energy drink) and (30 wt% IL + 30 wt% PPG400 + 40 wt% expired energy drink). The
227 mixture compositions were chosen taking into account two common mixture points in the
228 biphasic region of all systems, while varying the IL and PPG 400 contents to address their
229 effects. Each biphasic system was prepared in 2 mL micro-centrifuge tubes by adding the
230 appropriate amount of PPG 400, IL and energy drink sample to make up a final weight of
231 1 g. It should be remarked that a liquid energy drink sample is being used directly in the
232 creation of ABS, thus allowing the integration of the extraction and purification steps.
233 Furthermore, by using designed ILs with similar chemical structures to the target
234 compounds, the recovery step can be avoided, allowing to develop and integrated
235 extraction-purification-recovery strategy. All systems were mixed vigorously using a
236 vortex agitator (Reax Top, Heidolph, Germany) and left at 25 °C for 2 h. Each ABS was

237 then centrifuged for 5 min at 2000 rpm to ensure the complete phase separation. The
238 weights of the top and bottom phases were measured.

239 Recovery efficiencies of studied molecules ($RE\%$) correspond to the percentage ratio
240 between the amount of each biomolecule in a given phase (IL- or PPG-rich) and that in
241 the total mixture, determined according to Eqs (1) and (2):

242

$$244 \quad RE_{IL} (\%) = \frac{[C]_{IL} \cdot w_{IL}}{m_0} \times 100 \quad (1)$$

243

$$245 \quad RE_{PPG} (\%) = \frac{[C]_{PPG} \cdot w_{PPG}}{m_0} \times 100 \quad (2)$$

251

246 where w_{IL} , w_{PPG} , $[C]_{IL}$ and $[C]_{PPG}$ are the weights of the IL- and PPG-rich phases and the
247 concentration of each biomolecule in the IL- and PPG-rich phases, respectively; m_0
248 corresponds to the mass of each biomolecule present in the overall ABS. At the conditions
249 used in this work, the top phase corresponds to the PPG-rich phase while the bottom phase
250 corresponds to the IL-rich phase.

252 According to the product label, the used energy drink contains ca. 320 mg.L⁻¹ of caffeine,
253 4000 mg.L⁻¹ of taurine and 80 mg.L⁻¹ of niacin. The amount of each studied alkaloid
254 (caffeine, niacin and taurine) in Red Bull was confirmed by HPLC using the respective
255 standards and calibration curves. The experimentally determined amounts of these
256 compounds are in accordance with the amounts labelled in the energy drink sample
257 (Figure S9 in the Supporting Information). The stability of caffeine, niacin and taurine in
258 the ABS phases after extraction was also evaluated by HPLC (Figure S10 in the
259 Supporting Information).

260 Caffeine and niacin in each ABS were quantified by HPLC-DAD. The HPLC analysis
261 was performed using an Agilent 1100 liquid chromatograph (USA) with a Zorbax XDB-
262 C18 column (4.6 mm × 250 mm, 3.5 μm particle size). The mobile phase was composed
263 of 18% methanol and 82% water, at a flow rate of 1.5 mL.min⁻¹, with an injection volume
264 of 20 μL and temperature oven at 25°C. Quantification was carried out at 273 nm for
265 caffeine and at 261 nm for niacin. The system was controlled by the Chemstation
266 software. The taurine concentration was determined by HPLC including a pre-column
267 derivatization with DNFB due to low absorption of taurine in the UV-Vis region. The
268 procedure of derivatization is described elsewhere.^{46, 47} Briefly, 100 μL of the sample,
269 200 μL of the 0.01 M carbonate buffer (pH 9), 500 μL of DMSO and 10 μL of DNFB
270 were added into an Eppendorf tube, vigorously mixed using a vortex agitator at 2500 rpm
271 for 30 s and placed in a water bath at 40 °C for 15 min. Then, 650 μL of 0.01 M phosphate
272 buffer (pH 6) was added. The mobile phase was a mixture of 0.01 M phosphate buffer pH
273 6 (A) and acetonitrile (B) and the following gradient profile was run: 0–10 min, 90% A
274 and 10% B; 10–15 min, 75% A and 25% B; 15–19 min, 50% A and 50% B; from 19 min,
275 90% A and 10% B at flow rate of 1 mL min⁻¹ with a sample injection volume of 20 μL
276 and detection wavelength at 360 nm.

277

278 **RESULTS AND DISCUSSION**

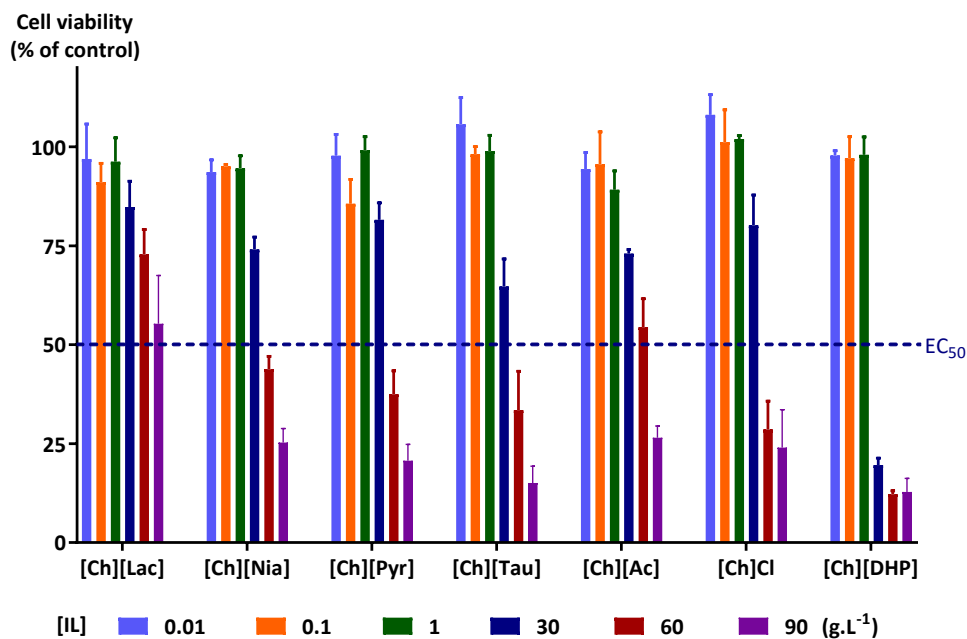
279 In this work, cholinium-based ILs with anions presenting similar characteristics to the
280 ones of the target high-value compounds, to recover from expired energetic drinks, were
281 synthesized and characterized. The ILs were then applied in the creation of ABS to
282 simultaneously extract and recover these compounds directly from the real samples. The
283 ILs selection was based on the premise that the IL-rich phase will have a superior
284 selectivity to the target compounds and that the activity of the recovered compounds could

285 be enhanced, while avoiding a final step to recover these target compounds from the IL-
286 rich phase. The ILs correspond to [Ch][Lac], [Ch][Nia], [Ch][Tau] and [Ch][Pyr]. Three
287 commercial ILs, namely, [Ch][DHP], [Ch][Ac], [Ch]Cl, were also used for comparison
288 purposes. The chemical structures of the investigated ILs and target added-value
289 compounds are depicted in Figure 1.

290

291 **ILs toxicity**

292 Given the potential applications of the recovered ABS phases containing the target
293 bioactive compounds, it is crucial to evaluate the ILs cytotoxicity. For this purpose, the
294 epithelial human colon cell line (Caco-2) was used to study the intestinal cytotoxic effects
295 of the investigated ILs. Figure 2 depicts the cytotoxic profile for the newly synthesized
296 ([Ch][Lac], [Ch][Nia], [Ch][Pyr], [Ch][Tau]) and the commercial ([Ch][Ace], [Ch]Cl and
297 [Ch][DHP]) ILs. The respective dose-response curves and the EC₅₀ values are shown in
298 the Supporting Information. Overall, the ILs investigated exhibit EC₅₀ values in the g.L⁻¹
299 range. [Ch][Lac] has the lowest toxicity (EC₅₀: 96.64 g.L⁻¹; 95% Confidence Interval
300 (CI): 74.95-118.3 g.L⁻¹), followed by [Ch][Pyr] (EC₅₀: 62.61 g.L⁻¹; 95% CI: 54.15-71.08
301 g.L⁻¹) and [Ch][Nia] (EC₅₀: 57.59 g.L⁻¹; 95% CI: 53.25-62.32 g.L⁻¹). Similar results were
302 obtained for the commercial IL [Ch][Ac] with an EC₅₀ of 65.11 g.L⁻¹ (95% CI: 56.29-
303 73.93 g.L⁻¹). [Ch][Tau] exhibits the highest cytotoxicity amongst the synthesized ILs
304 (EC₅₀: 30.05 g.L⁻¹; 95% CI: 29.67-30.43 g.L⁻¹), being comparable with the ones obtained
305 for the commercial ILs [Ch]Cl (EC₅₀: 30.61 g.L⁻¹; 95% CI: 29.85-31.36 g.L⁻¹) and
306 [Ch][DHP] (EC₅₀: 28.97 g.L⁻¹; 95% CI: 28.50-29.44 g.L⁻¹). The toxicity of [Ch][Tau] is
307 approximately twice as high as [Ch][Pyr], [Ch][Nia] or the commercial [Ch][Ac]. A
308 similar profile was obtained for the ecotoxicity tests, with [Ch][Tau] showing the highest
309 toxicity (results and discussion below).



310

311 **Figure 2.** Caco-2 cell viability after 24 h of exposure to the ILs (average values with
 312 respective standard error). The dashed line corresponds to the EC₅₀.

313

314 In addition to the cytotoxicity, the ecotoxicity of the synthesised ILs was addressed using
 315 the bioluminescent bacteria *Vibrio fischeri*. The experimental EC₅₀ values were
 316 determined by Microtox® bioassays for 5, 15 and 30 min of IL exposure. The detailed
 317 results are provided in the Supporting Information. According to the Passino's
 318 classification⁴⁸, the obtained results reveal that [Ch][Nia] is harmless (EC₅₀ > 1000 mg.L⁻¹)
 319 ¹), [Ch][Lac] is practically harmless (100 mg.L⁻¹ < EC₅₀ > 1000 mg.L⁻¹) and [Ch][Tau] is
 320 moderately toxic (10 mg.L⁻¹ < EC₅₀ > 100 mg.L⁻¹). [Ch][Pyr] has non-toxic character to
 321 the addressed bacteria given that at 60 mg.L⁻¹ concentration it was not possible to
 322 calculate the EC₅₀ value. These results suggest that the investigated anions have a relevant
 323 role in defining the cholinium-based ILs toxicity, in agreement with the findings of
 324 Ventura et al.⁴⁹ showing that [Ch][Ac], [Ch]Cl and [Ch][DHP] are “practically harmless”
 325 with EC₅₀ values after 30 min of exposure of 673.21 mg.L⁻¹ for [Ch][Ac], 469.34 mg.L⁻¹
 326 for [Ch]Cl and 572.72 mg.L⁻¹ for [Ch][DHP]. [Ch][Tau] is more toxic than these

327 commercial ILs. However, [Ch][Lac] is less toxic than [Ch]Cl and has a similar toxicity
328 to [Ch][DHP] and [Ch][Ac]. [Ch][Nia] and [Ch][Pyr] are less toxic than all commercial
329 ILs investigated. Overall, most of the studied ILs have a low environmental impact, where
330 [Ch][Nia] and [Ch][Pyr] stand out as less toxic cholinium-based ILs than those
331 commercially available. This feature is even more relevant if considering the largely
332 investigated imidazolium-based ILs in ABS for separation purposes.¹⁵

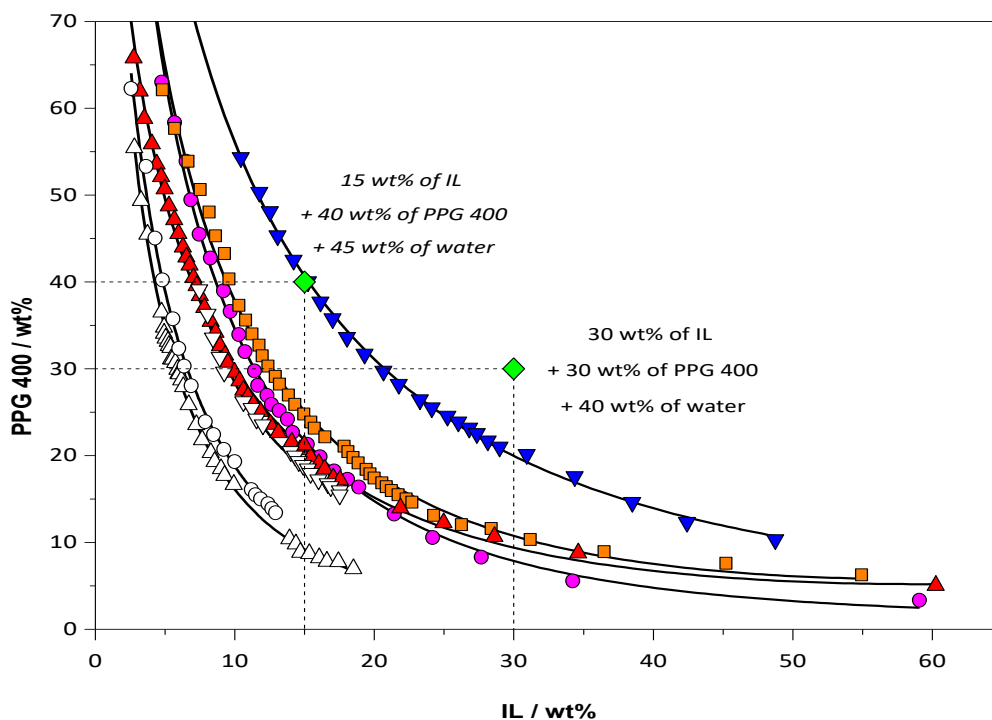
333

334 **ABS phase diagrams and extraction and recovery of added-value compounds from** 335 **expired energy drinks**

336 By using expired energy drinks, which are liquid samples, to directly create ABS, it is
337 possible to integrate the extraction and recovery steps of the target added-value
338 compounds. With this goal in mind, the ABS phase diagrams were first determined at
339 25°C and atmospheric pressure. The binodal curves experimental data for the ABS
340 composed of each IL, PPG 400 and water are given in the Supporting Information. The
341 respective phase diagrams, given in weight fraction, are shown in Figure 3. Each binodal
342 curve represents the minimum concentration of the system constituents required for the
343 formation of two aqueous phases at 25°C and atmospheric pressure. The binodal curve
344 data were fitted according to the equation proposed by Merchuk et al.,⁵⁰ being given in
345 Figure 3. Fitting parameters obtained from the correlation of experimental data and
346 corresponding correlation coefficients are provided in the Supporting Information.

347 Considering that PPG 400 and the cholinium cation are common species to all
348 investigated ABS, the two-phase forming ability of each system is a main result of the IL
349 anion chemical structure. The closer the binodal curve is to the origin of the phase
350 diagram, the lower the concentrations of phase-forming components required for the
351 formation of ABS. The phase-forming ability of the studied ILs in ABS formation, at ca.

352 25 wt% of PPG 400, follows the order: [Ch][DHP] > [Ch][Ac] > [Ch]Cl > [Ch][Tau] >
 353 [Ch][Lac] > [Ch][Pyr] > [Ch][Nia]. [Ch][DHP] shows the highest ability to form ABS,
 354 whereas [Ch][Nia] exhibits the lowest.



355
 356 **Figure 3.** Ternary phase diagrams of the studied ABS (IL + PPG400 + H₂O) at 25°C and
 357 atmospheric pressure: Δ , [Ch][DHP]; \circ , [Ch][Ac]; ∇ , [Ch]Cl; \blacktriangle , [Ch][Tau]; \bullet ,
 358 [Ch][Lac]; \blacksquare , [Ch][Pyr] and \blacktriangledown , [Ch][Nia]. \blacklozenge , ABS compositions used in the extraction
 359 studies; continuous line, fitting of the experimental binodal data.

360
 361 According to the given trend, it seems that the cholinium-based ILs act as the salting-out
 362 species over the moderately hydrophobic PPG 400. The salting-out aptitude of ILs is
 363 directly related to the hydration capacity of their ions.^{32, 51} Since all ILs share a common
 364 cation, cholinium, more hydrophilic anions with a higher charge density, such as [DHP]⁻
 365 , have a higher hydration ability and display stronger salting-out effects. However, it
 366 should be taken into account that the mechanisms behind the formation of ABS containing

367 ILs and polymers are far more complex than those observed in ABS formed by salts and
368 ILs.⁴⁵ It was previously reported that the ABS formation in systems comprising higher
369 melting temperature cholinium-based ILs, e.g. [Ch][DHP], [Ch][Ac] and [Ch]Cl, is
370 mainly governed by their affinity for water.⁵² A higher affinity for water implies a higher
371 ability to promote phase separation when dealing with systems involving polymers, where
372 the ILs acts as the salting-out species. In the case of ABS based on ILs with lower melting
373 temperatures (which will be the case of [Ch][Tau], [Ch][Lac], [Ch][Pyr] and [Ch][Nia])
374 and polymers, the two-phase formation ability is not a main result of the IL ions to create
375 hydration complexes, but yet the IL-polymer interactions play a significant role.⁵³
376 The anions hydrophobicity may be appraised by the logarithmic values of their octanol-
377 water partition coefficients ($\log K_{ow}$); for conjugated acids of the studied anions they are
378 in the range from -2.77 to 0.22 (detailed values given in the Supporting Information).
379 The most hydrophilic anion is [Tau]⁻, justifying its higher affinity for water and salting-
380 out ability. On the other hand, the most hydrophobic anion is [Nia]⁻, which shows the
381 lowest ability to form ABS. However, the obtained trend of ABS formation does not
382 straight follow the $\log K_{ow}$ values; according to this rank, [Ch][Pyr] ($\log K_{ow} = -1.24$)
383 should be a stronger salting-out agent than [Ch][Lac] ($\log K_{ow} = -0.70$). On the other hand,
384 the trend of low melting cholinium-based ILs to induce ABS follows the decrease in the
385 anion polar surface, which is the surface sum over all polar atoms (80.39, 60.36, 57.20
386 and 50.19 \AA^2 for [Ch][Tau], [Ch][Lac], [Ch][Pyr] and [Ch][Nia], respectively).⁵⁴ These
387 results suggest that the ABS formation of these low melting ILs with PPG is governed by
388 their ability to be solvated by water to act as salting-out species and by specific
389 interactions with the polymer, being in agreement with the literature.⁵² For instance,
390 [Ch][Nia] contains π electrons able to establish strong hydrogen bond interactions with

391 the ether oxygen atoms of PPG, and this could be the major factor for the lower ability of
392 [Ch][Nia] to promote the creation of ABS with PPG.

393 Tie-line (TL) compositions, tie-lines length (TLL) and slope were additionally
394 determined for ABS formed with the synthesized ILs, being given in the Supporting
395 Information. TL data are particularly relevant to have information on the compositions of
396 the phases at which the extractions are carried out.

397 After addressing the phase-forming components compositions required to create ABS,
398 the potential of these new ABS formed by cholinium-based ILs and PPG 400 to recover
399 added-value compounds from expired energy drinks, namely caffeine, taurine and niacin
400 (Vitamin B₃), was investigated. The synthesized ILs were designed to have similar anions
401 to the target products, which could be beneficial to improve selectivity and biological
402 activity while ideally avoiding the need of the products recovery from the ABS phases.

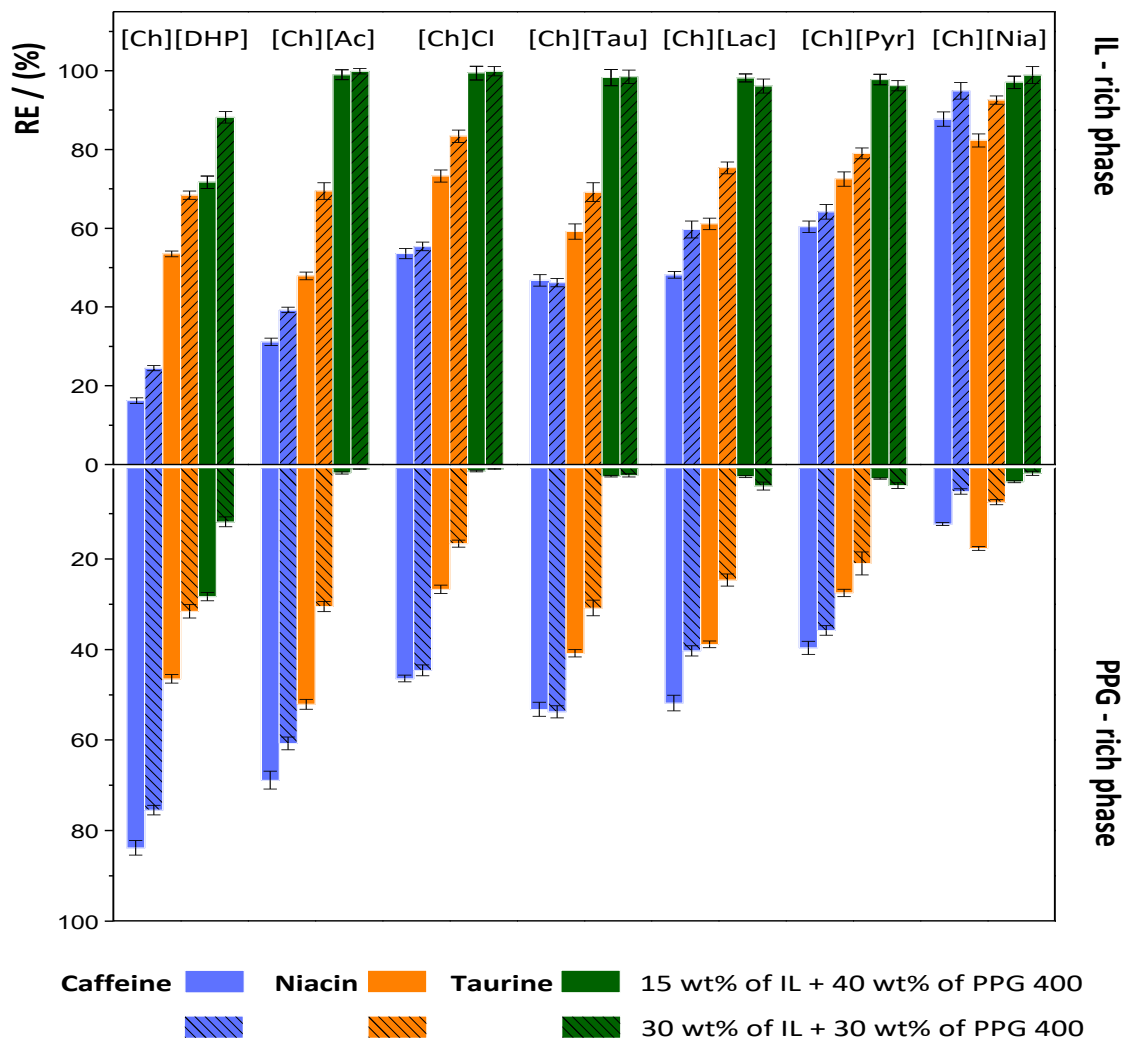
403 The commercial energy drink contains aspartame, acesulfame K (110 g.L⁻¹), caffeine (320
404 mg.L⁻¹), taurine (4 g.L⁻¹), vitamin B₃ - niacin (80 mg.L⁻¹) and other B complex vitamins
405 (Figure S9 in the Supporting Information). The properties of the targeted compounds
406 which can influence the partitioning in the proposed ABS and their stability in the ABS
407 phases are given in the Supporting Information (Table S6 and Figure S10, respectively).

408 All studied bioactive compounds are stable in the ABS' phases and ILs/PPG 400 aqueous
409 solutions. According to the chromatograms given in Figure S10 in the Supporting
410 Information, it is shown that the retention times of taurine, niacin and caffeine do not
411 change when compared to the standards and that no new peaks appear in addition to those
412 already existing in the energy drink sample.

413 The extraction of the target compounds from the energy drink was performed at two
414 ternary system compositions (identified in Figure 3): (A) 15 wt% of IL, 40 wt% of PPG
415 400 and 45 wt% of expired energy drink, and (B) 30 wt% of IL, 30 wt% of PPG 400 and

416 40 wt% of expired energy drink. The composition of the ternary mixtures was selected
417 based on the phase diagrams previously determined, and close to the binodal curve of the
418 ABS with lowest ability to undergo liquid-liquid demising aiming at improving their
419 sustainability, i.e. requiring lower amounts of the phase-forming components (IL and
420 PPG 400). The obtained recovery efficiencies (*RE%*) in the IL-rich and PPG-rich phases
421 for niacin, caffeine and taurine are depicted in Figure 4 (detailed results are provided in
422 the Supporting Information).

423 At the conditions investigated, taurine and niacin from the expired drink preferentially
424 migrate to the IL-rich phase in all ABS, whereas caffeine shows an opposite pattern in
425 most of the systems investigated (preferential migration towards the PPG-rich phase, with
426 the exception of [Ch][Pyr]-, [Ch][Nia]- and [Ch]Cl-based ABS) – *cf.* Figure 4. Recovery
427 efficiencies varying from 47.89 to 92.55% for niacin and from 71.68 to 99.87% for taurine
428 to the IL-rich phase, and varying between 5.12 to 83.81% for caffeine to the PPG-rich
429 phase, were obtained. These values support the ILs designer aptitude since the almost
430 complete extraction of the three target compounds is achieved in one-step into the IL-rich
431 phase with the ABS formed by [Ch][Nia], whereas the ABS formed by [Ch][DHP] allows
432 to separate niacin and taurine from caffeine (by their partitioning to opposite phases).



433

434 **Figure 4.** Recovery efficiencies of the caffeine, niacin and taurine in the studied ABS at
 435 two mixture compositions at 25°C.

436

437 Caffeine can be used as an effective and valuable probe to characterize the relative
 438 hydrophobicity of a series of ABS, particularly when hydrophobic type interactions are
 439 predominant, since this alkaloid does not suffer speciation in a large range of pH values
 440 ($pK_{a1}/pK_{a2} = 0.12 / 10.5$) while being moderately hydrophilic ($\log K_{ow} = -0.63$).⁵⁵
 441 According to the $RE\%$ values, caffeine preferentially partitions to the PPG-rich phase at
 442 both compositions, except in the case of the ABS composed of [Ch][Nia] and [Ch][Pyr]

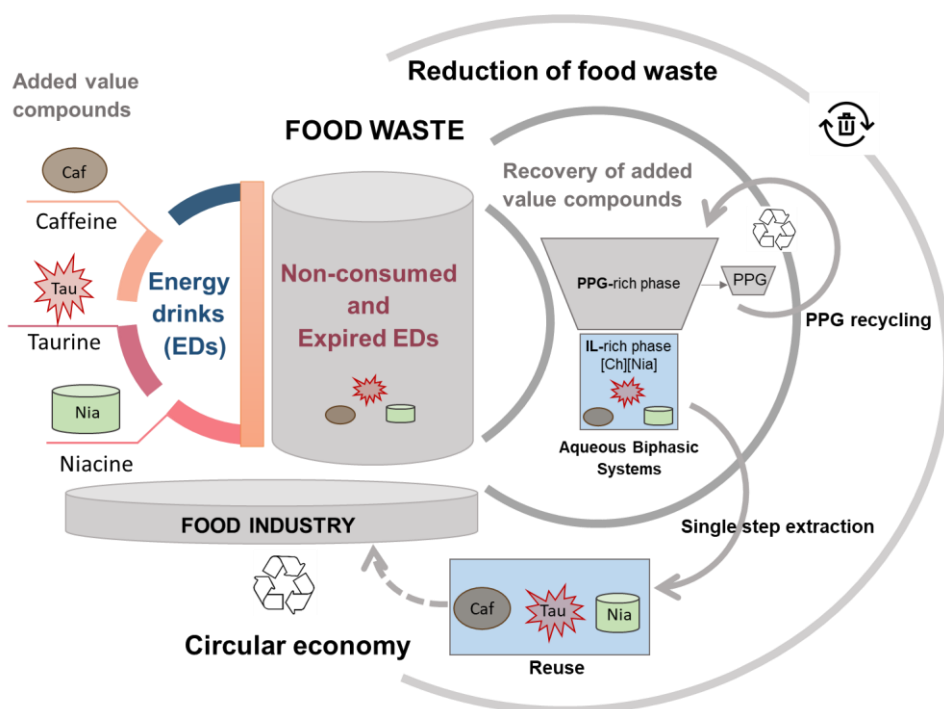
443 where caffeine preferentially migrates to the IL-rich phase (Figure 4). Recovery
444 efficiencies of caffeine in the range from 16.19 to 55.38% toward the IL-rich phase and
445 from 5.12 to 83.81% to the PPG-rich phase were obtained, meaning that the enrichment
446 of caffeine in a given phase can be tailored by changing the IL chemical structure. In ABS
447 composed of [Ch][DHP], [Ch]Cl and [Ch][Ac], caffeine is majorly enriched in the PPG-
448 rich phase. On the other hand, when more hydrophobic ILs are applied, such as [Ch][Pyr]
449 and [Ch][Nia], caffeine preferentially partitions to the IL-rich phase. It should be noted
450 that the water content in the PPG400-rich phase in the ABS based on [Ch][Pyr] and
451 [Ch][Nia] is significantly low (3.13-20.52 wt% and 1.85-15.85 wt%, respectively)
452 compared to ABS based on [Ch][Tau] (20.04-33.79%) and [Ch][DHP]⁵⁶ (17.16-35.87%)
453 (cf. the Supporting Information, tie-line data), thus justifying the inversion on the caffeine
454 partitioning among the coexisting phases, and in agreement with the use of caffeine as a
455 valuable probe to characterize the relative hydrophobicity of ABS phases.⁴⁹

456 Niacin (pKa=4.80)⁵⁷, unlike caffeine, is negatively charged in the pH range of the studied
457 ABS (5.8-10.1). Moreover, niacin is the most hydrophilic compound (logK_{ow} values
458 ranging from -2.03 to -2.93 in the pH range 5.8-10.1) and contains an acidic (-COOH)
459 and a basic group (N from the pyridine core. In the same line, taurine (pKa=-1.49 /9.06)⁵⁷
460 has a high hydrophilic nature (logK_{ow} values ranging from -5.27 to -6.23 in the pH range
461 5.8-10.1), and exists as a zwitterion or as negatively charged species at the working pH.
462 The results disclosed in Figure 4 show that niacin and taurine preferentially migrate to
463 the IL-rich phase, which is the most hydrophilic phase in the ABS phases, mainly due to
464 their hydrophilic character.

465 In summary, the ABS evaluated are able to remarkably recover added-value compounds
466 directly from expired energy drinks. Furthermore, caffeine, taurine and niacin can be
467 recovered in one phase or caffeine can be separated from the remaining target compounds

468 only by changing the IL chemical structure. For the first strategy, the best ABS is formed
469 by [Ch][Nia] that allows to recover all compounds in one step with *RE%* higher than
470 82.32%, whereas the best ABS able to separate caffeine from taurine and niacin is
471 composed of the commercial IL [Ch][DHP]. [Ch][Nia] exhibits low cytotoxicity and low
472 ecotoxicity, while PPG 400 is approved as a food additive by FDA.⁵⁸ Given the
473 envisioned target applications and assuming that no separation of caffeine from taurine
474 and niacin is aimed, the results obtained reveal that the ABS formed by [Ch][Nia] and
475 PPG 400 is the most efficient system to recover added-value compounds from expired
476 energy drinks, which could be then reused in diverse industrial applications without the
477 need of removing the IL or recovering the target compounds from the IL-rich phase. For
478 instance, these compounds can be used together in food supplements and in cosmetic or
479 pharmaceutical formulations. Despite our promising results, it should be stressed that a
480 thorough risk assessment is required in order to demonstrate the safety use of the IL-rich
481 phase directly by these industries. This assessment includes further *in vitro* and *in vivo*
482 tests in order to evaluate the acute and chronic toxicity towards mammals and towards
483 other test organisms from different trophic levels to guarantee that there are no hazards
484 related with these products.

485 A schematic overview of the developed integrated platform, and within a circular
486 economy perspective, to extract and recover added-value compounds from expired
487 energy drinks without the need of recovering them from the IL-rich phase is shown in
488 Figure 5. This strategy envisions the direct use of the IL-rich fraction with enhanced
489 biological activity by the food, cosmetics or pharmaceutical industries, although
490 additional tests are required as highlighted above. The reuse of the PPG-rich phase is also
491 envisioned, particularly in the creation of a new ABS with similar samples, at least up to
492 saturation or losses of separation performance.



494

495 **Figure 5.** Schematic representation of the proposed integrated platform to extract and
 496 recover added-value compounds from expired energy drinks using ABS composed of
 497 cholinium-based ILs and PPG 400.

498

499 CONCLUSIONS

500 In this work, we proposed an integrated approach to extract and recover high-value and
 501 bioactive compounds from expired energy drinks using aqueous biphasic systems
 502 composed of cholinium-based ILs and PPG 400. A set of cholinium-based ILs was
 503 synthesized, characterized and used. [Ch][Lac] exhibits the lowest toxicity towards the
 504 human epithelial colon cell line (Caco-2), followed by [Ch][Pyr] and [Ch][Nia].
 505 [Ch][Tau] exhibits the highest cytotoxic character, being comparable to the commercial
 506 ILs [Ch]Cl and [Ch][DHP]. A similar profile with [Ch][Tau] exhibiting the highest

507 toxicity was obtained for the ecotoxicity tests, with this IL being considered moderately
508 toxic. [Ch][Nia] is harmless to the marine bacteria *V. fischeri*, whereas [Ch][Lac] and
509 [Ch][Pyr] were considered as practically harmless.

510 The ABS phase diagrams were determined at 25°C and atmospheric pressure, in which
511 the ILs in ABS formation followed the order: [Ch][DHP] > [Ch][Ac] > [Ch]Cl >
512 [Ch][Tau] > [Ch][Lac] > [Ch][Pyr] > [Ch][Nia]. In the studied ABS, taurine and niacin
513 preferentially migrate to the IL-rich phase, while caffeine migrates in the majority of the
514 cases towards the PPG-rich phase. However, an opposite behaviour on the partition of
515 caffeine was achieved with ABS formed by [Ch][Pyr] or [Ch][Nia], in which caffeine
516 also partitions to the IL-rich phase. The system composed of [Ch][Nia] and PPG 400
517 allows the almost complete recovery ($RE\% > 82.32\%$) of all the target compounds into
518 the IL-rich phase in one-step. Given that [Ch][Nia] exhibits lower cytotoxic potential and
519 is considered harmless from an ecotoxicological point of view, this system can be
520 considered a promising platform to simultaneously extract, recover and reuse added-value
521 compounds from expired energy drinks and thus contribute to a more sustainable and
522 circular food economy.

523

524 **ASSOCIATED CONTENT**

525 **Supporting Information.** Supplementary Information available: [NMR and FTIR
526 spectra; information on the determination of the ABS phase diagrams; Caco-2
527 cytotoxicity dose response curves; Microtox toxicity results; Ternary phase diagrams and
528 binodal weight fraction data of ABS, TLs and TLLs; HPLC chromatograms; Recovery
529 efficiencies].

530

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535 **Notes**

536 There are no conflicts to declare.

537 **ACKNOWLEDGMENT**

538 This work was developed within the scope of the project CICECO-Aveiro Institute of
539 Materials, UIDB/50011/2020 & UIDP/50011/2020, financed by national funds through
540 the FCT/MEC and when appropriate co-financed by FEDER under the PT2020
541 Partnership Agreement. A.C.A.S. acknowledges Universidade de Aveiro for funding in
542 the scope of the framework contract foreseen in the numbers 4, 5 and 6 of the article 23,
543 of the Decree-Law 57/UIDB/50011/2020 & UIDP/50011/20202016, of August 29,
544 changed by Law 57/2017, of July 19. Ana P. M. Tavares acknowledges FCT for the
545 Investigator Programme (IF/01634/2015). Additional support was provided by project
546 FCT ref. UID/Multi/00709/2019 and the Ministry of Education, Science and
547 Technological Development of Serbia under project contracts III 45006 and ON 172012.

548

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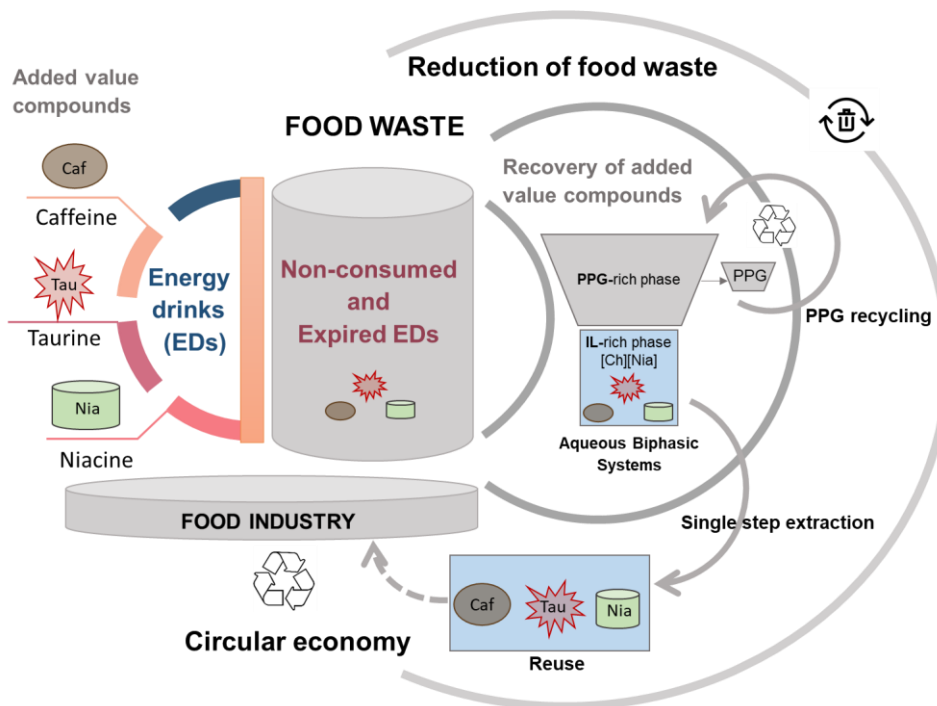
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696 Ionic-liquid-based aqueous biphasic systems are effective platforms to simultaneously
 697 extract, recover and reuse added-value compounds from expired energy drinks,
 698 contributing to a sustainable and circular food economy.

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