

## Supporting information

# Modelling hydrate dissociation curves in the presence of hydrate inhibitors with a modified CPA EoS.

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Table S1 – Absolute average deviations (%) for pressures, in Pa, of the systems water with methanol, ethanol.

water : methanol				water : ethanol			
T/K	Ref.	P <sub>bub</sub>	P <sub>dew</sub>	T/K	Ref.	P <sub>bub</sub>	P <sub>dew</sub>
323	<sup>1</sup>	2.37	0.98	298	<sup>2</sup>	3.36	2.59
328	<sup>1</sup>	2.60	1.22	313	<sup>3</sup>	6.09	0.88
333	<sup>1</sup>	3.04	2.13	363	<sup>4</sup>	1.40	4.18
363	<sup>5</sup>	4.85		381	<sup>4</sup>	1.65	2.73
383	<sup>5</sup>	3.86		403	<sup>4</sup>	2.91	2.69
403	<sup>5</sup>	5.30		423	<sup>4</sup>	2.43	1.51
424	<sup>5</sup>	2.75		473	<sup>6</sup>	0.75	
442	<sup>5</sup>	6.53		473	<sup>7</sup>	2.31	1.46
				523	<sup>6</sup>	1.12	
				523	<sup>7</sup>	0.97	0.62
				548	<sup>6</sup>	0.49	
				548	<sup>7</sup>	1.59	0.59
				573	<sup>6</sup>	1.83	0.99

Table S2 – Absolute average deviations (%) on mole fractions of the systems water with methanol, ethanol.

water : methanol				water : ethanol			
T/K	Ref.	y <sub>1</sub>	x <sub>1</sub>	T/K	Ref.	y <sub>1</sub>	x <sub>1</sub>
323	<sup>1</sup>	4.21	3.74	298	<sup>2</sup>	9.20	14.03
328	<sup>1</sup>	4.89	4.23	313	<sup>3</sup>	9.48	5.96
333	<sup>1</sup>	5.19	4.14	363	<sup>4</sup>	10.63	14.52
				381	<sup>4</sup>	10.87	12.63
				403	<sup>4</sup>	14.06	11.17
				423	<sup>4</sup>	6.44	5.62
				473	<sup>6</sup>	2.10	1.79
				523	<sup>6</sup>	1.00	0.86
				548	<sup>6</sup>	0.93	1.37
				573	<sup>6</sup>	1.41	1.04

Table S3 – Compositions of the gases on section 3.3 of this work.

Gas/ Compound	% mol				
	mixture 1 <sup>8</sup>	natural gas <sup>9</sup>	sour gas 1 <sup>10</sup>	sour gas 2 <sup>10</sup>	sour gas 3 <sup>10</sup>
$N_2$	0	0.04	3.00	2.00	0.50
$H_2S$	0	0	3.49	6.96	9.47
$CO_2$	0	0	11.00	17.50	5.01
methane	91.00	89.86	82.51	73.54	85.02
ethane	9.00	6.40	0	0	0
propane	0	2.71	0	0	0
iso-butane	0	0.48	0	0	0
n-butane	0	0.49	0	0	0
iso-pentane	0	0	0	0	0
n-pentane	0	0.02	0	0	0

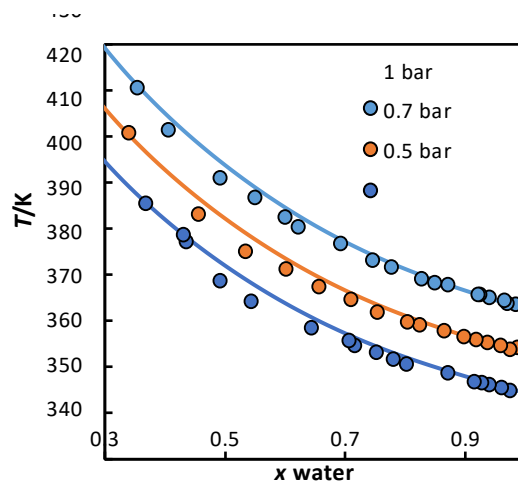


Figure S1 – VLE for water + triethylene glycol. Experimental data from Chouireb et al. <sup>11</sup>

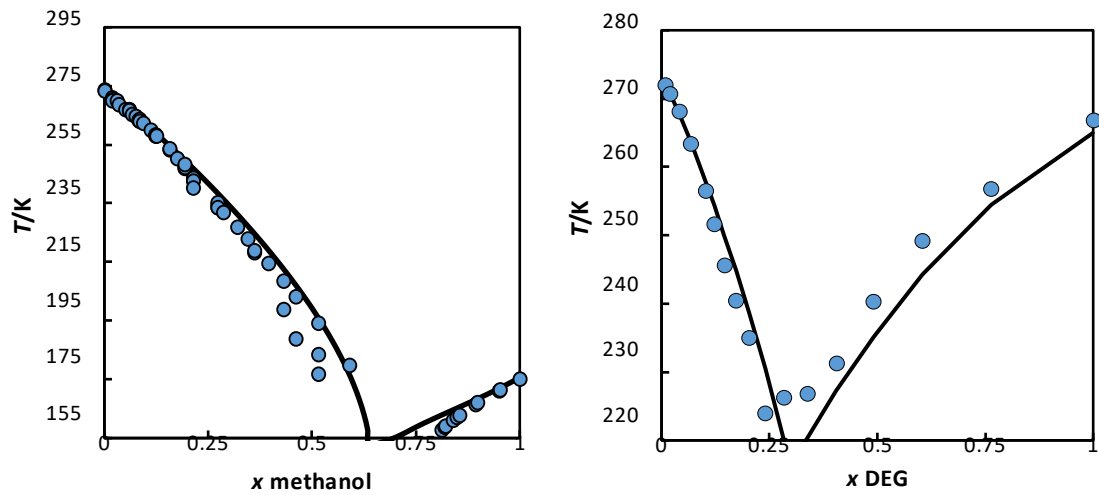


Figure S2 – SLE for water + methanol (left) and water + DEG (right). Experimental data from Chouireb et al.<sup>11</sup> and TRC.<sup>12</sup>

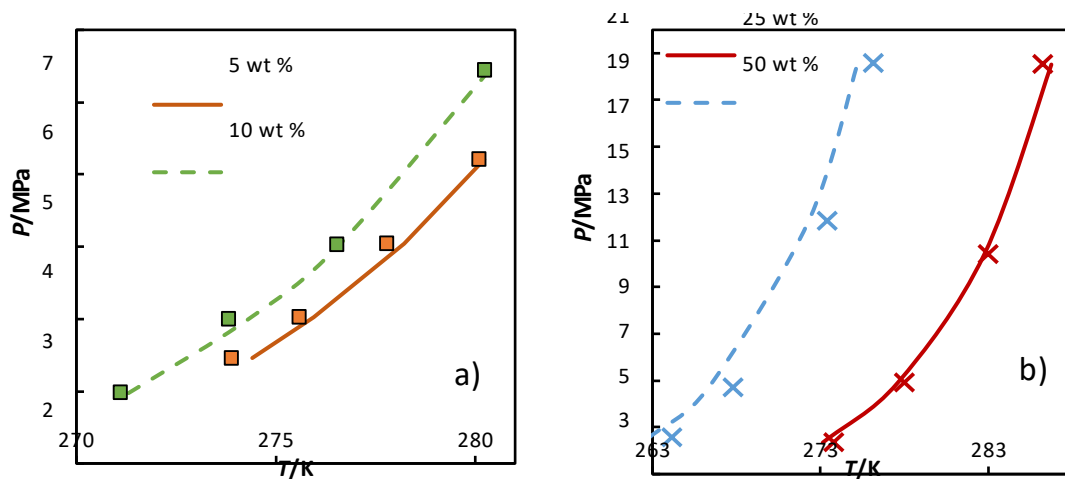


Figure S3 – Hydrate dissociation curves for mixtures of methane + water + inhibitor/guest hydrate former; Inhibitor/guest hydrate former a) ethanol, b) glycerol. wt % refers to weight percentage of inhibitor in aqueous solution.  $\square$  – Sloan and Koh<sup>13</sup>;  $\times$  – Ng and Robinson<sup>14</sup>;  $+$  – Youn et al.<sup>15</sup>.

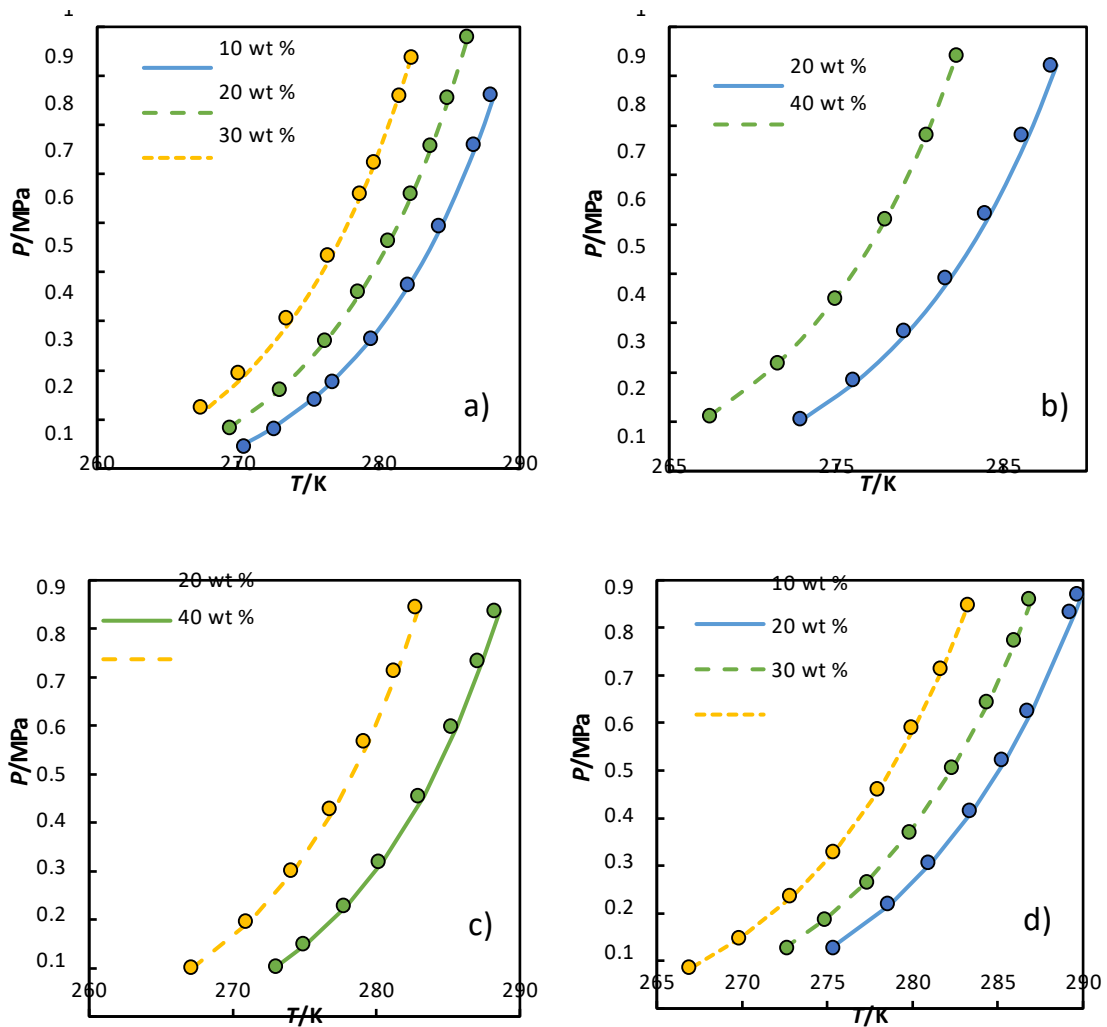


Figure S4 – Hydrate dissociation curves for mixtures of xenon + water + inhibitor; Inhibitor a) ethanol, b) glycerol, c) DEG, d) MEG. wt % refers to weight percentage of inhibitor in the aqueous phase. Single Lines – first sets; Double lines – second sets. ○ – Maekawa.<sup>16</sup>

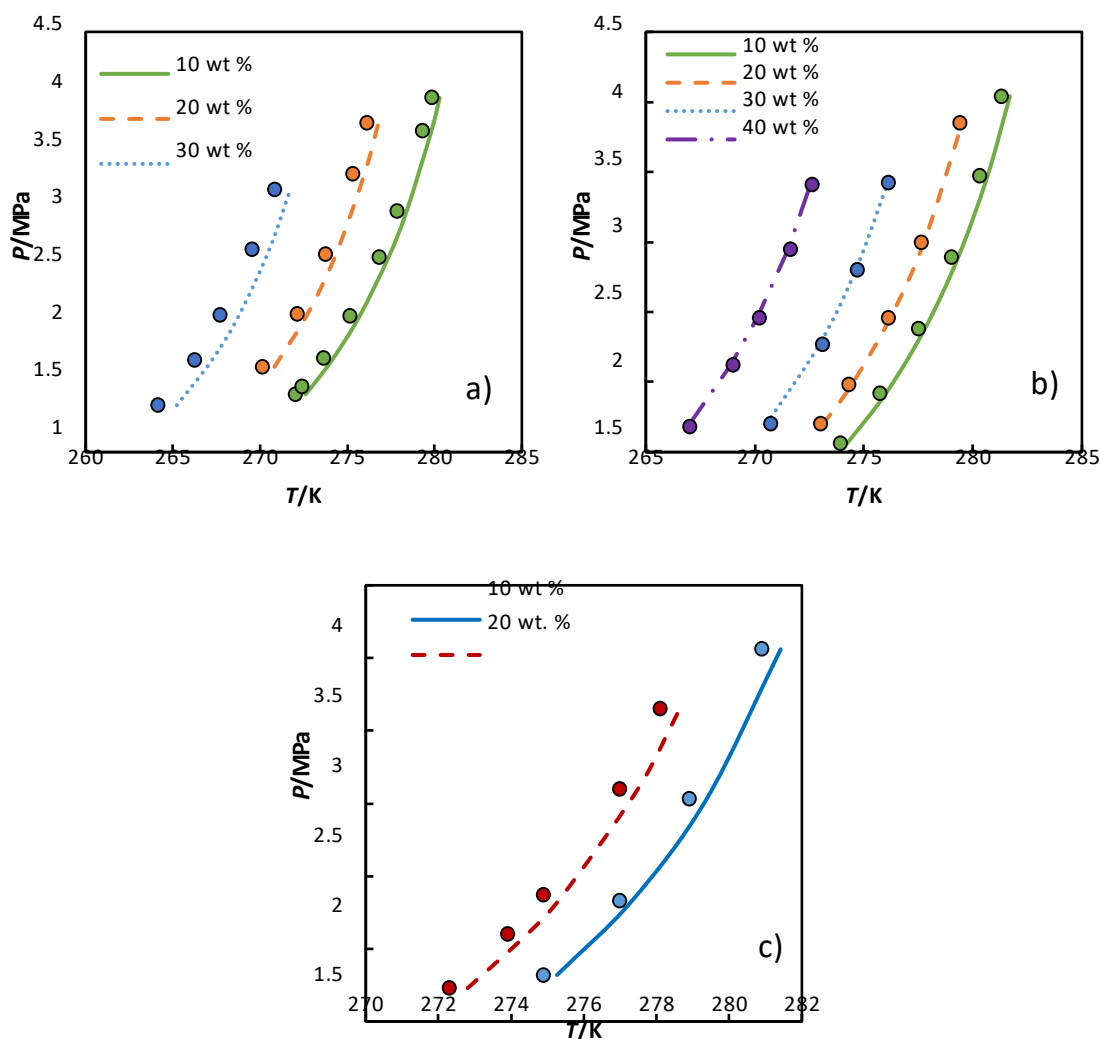


Figure S5 – Hydrate dissociation curves for mixtures of CO<sub>2</sub> + water + inhibitor; Inhibitor a) MEG, b) TEG c) DEG. wt % refers to weight percentage of inhibitor in aqueous solution. ○ – Maekawa.<sup>17</sup>

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